

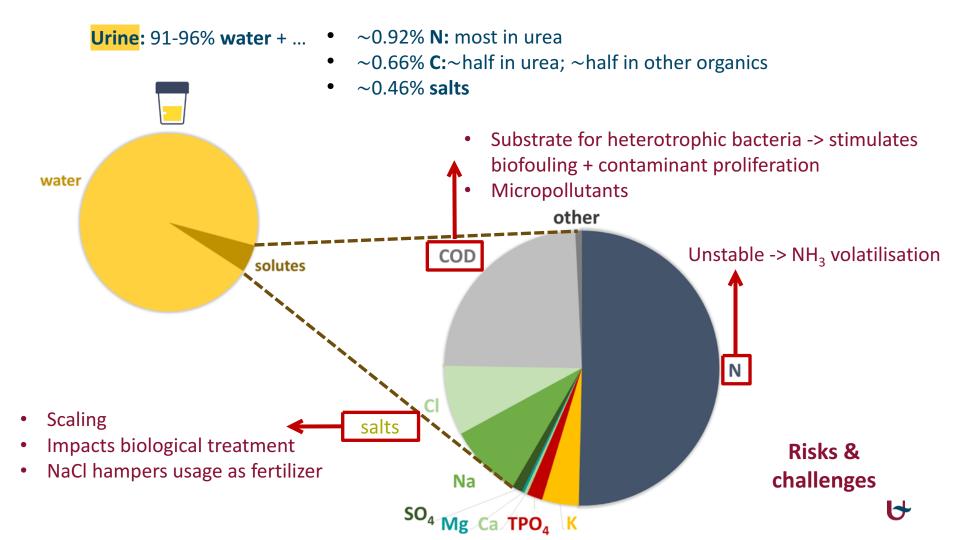
Nitrify for life: Sustainable solutions for Space and Earth

Siegfried Vlaeminck, Marc Spiller, Marijn J. Timmer,

Patricia Gutiérrez Lozano & Tim Van Winckel







Water in Space? Urine as major flow in missions without grey water

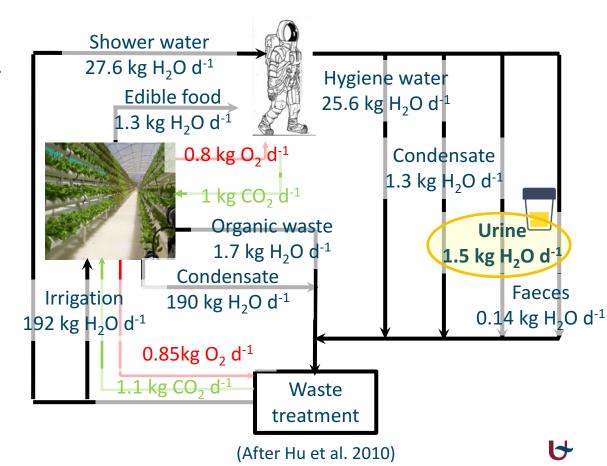
Short missions:

- Yellow water: Urine + flush water → around half of the water flow
- **Condensate:** Respiration and transpiration crew

Sabatier water, as a function of the CO₂ management system

Additional flows in longer missions:

- Grey water from hygiene activities (e.g. shower)
- Transpiration water (food production with plants)
- **Black** water (from toilet flush)
- Grey water from service activities (laundry, dish-washer, etc.)



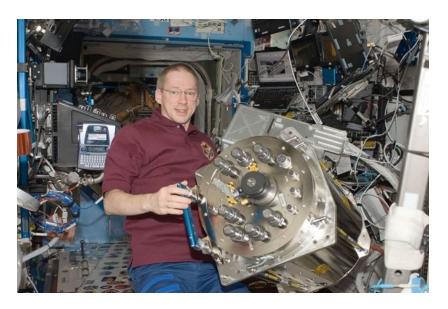
Water recovery from urine in Space?

In the International Space Station (ISS), Belgian astronaut Frank De Winne: "In Space, we drink the **same coffee every day!"**

-> Water recycling from urine is a no-brainer for human exploration



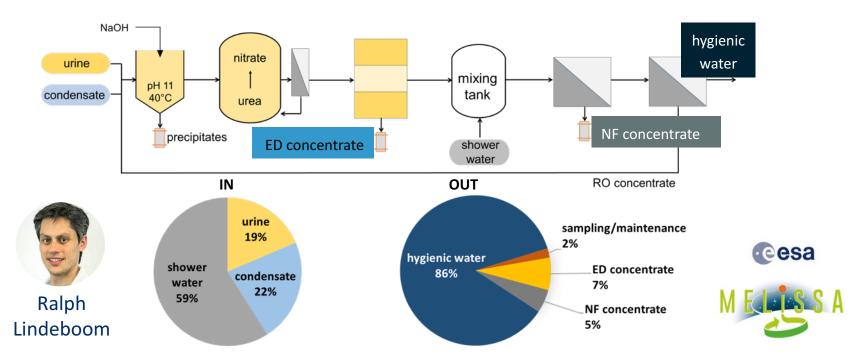
Racks for the ISS water recovery system (Carter et al. 2011)



Belgian astronaut Frank De Winne repairing the Urine Processor Assembly (UPA)



Water recovery enabled by nitrification: Water treatment unit breadboard (WTUB)



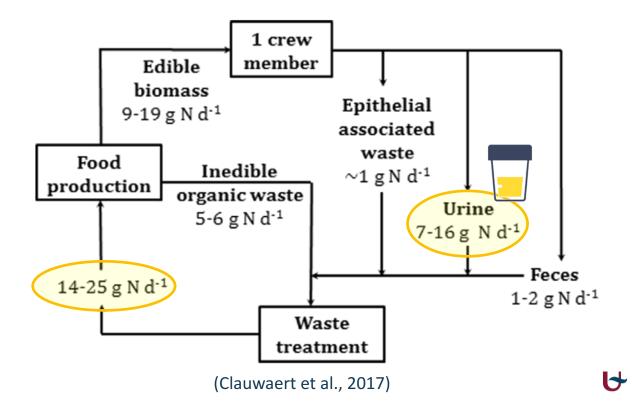
- Results of a 4-months breadboard operation campaign: total water recovery of 86%
- Reduced scaling potential with anti-scalant addition
- Stable but biofouling-limited RO permeability (0.5 L/m²/h/bar)

6

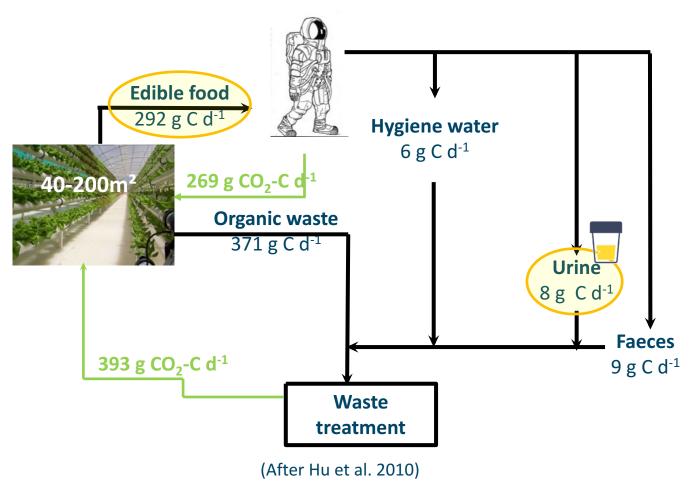


Nitrogen in Space? -> Urine as major flow

Urine: 50-64% in closed system with food production



Carbon in Space? -> **Urine** as **negligible** flow

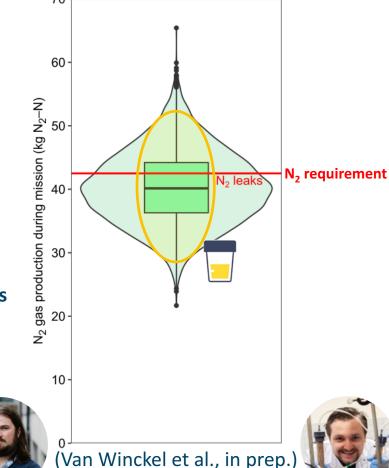




Nitrogen gas (N₂) requirements and production potential in Space

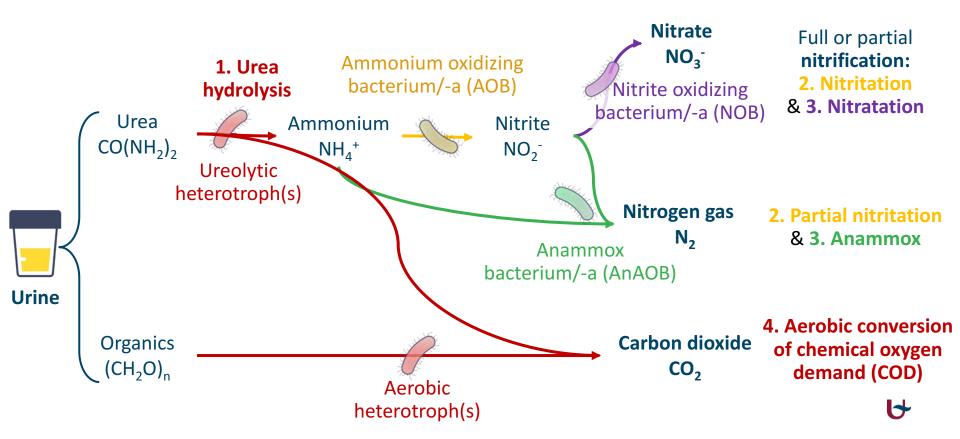
• N₂ requirement

- To maintain a pressurised cabin atmosphere, counteracting losses due to extravehicular activities, structural leakages,...
- 42.5 kg N needed
- Production potential of N₂ from urine
 - Through partial nitritation/anammox
 - 40.3 kg N produced on average
- N₂ recovery from urine offsets on average 95% of the N₂ gas needs (65% of the stochastic runs can offset all losses)
- Assumptions: Mars transit mission, 4 crew members, 850 days

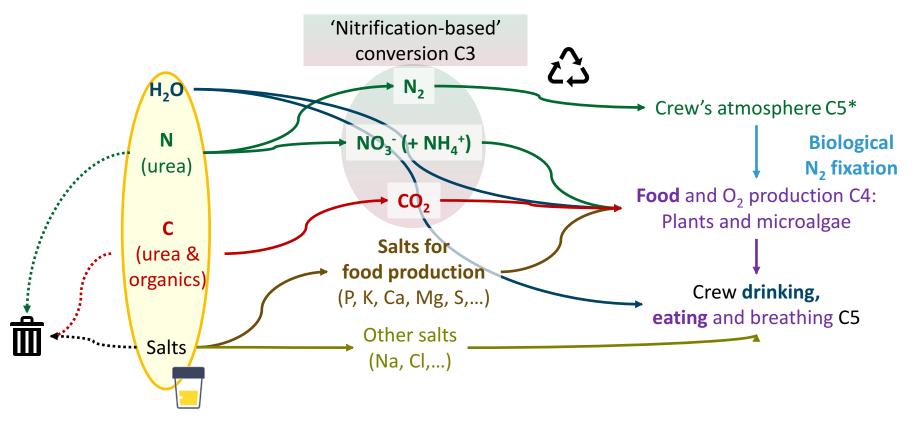


'Nitrification-based' conversions for N and C in urine: 2 routes, having 3 out of the 4 steps in common:

= Ureolysis AND (Partial) Nitritation AND (Nitratation OR Anammox) AND COD conversion



Modular and complimentary options to deal with urinary resources



Note: N₂ production can be an elegant solution to uncouple undesired salinity (NaCl) from water and useful nutrients for food production driven by biological N₂ fixation



N and C conversion stoichiometries in urine

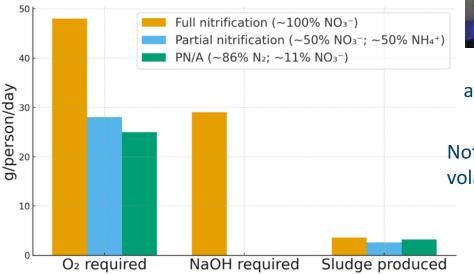
Combined processes	Overall stoichiometry	
Ureolysis, full nitrification & C conversion	$0.5 \text{ CO(NH}_2)_2 + 0.22 \text{ CH}_3 \text{COOH} + 2.18 \text{ O}_2$ \rightarrow 0.96 NO ₃ ⁻ + 0.036 C ₅ H ₇ O ₂ N + 0.76 CO ₂ + 1.06 H ⁺ + 0.73 H ₂ O	
Ureolysis, partial nitritation/anammox & C conversion	$0.5 \text{ CO(NH}_2)_2 + 0.22 \text{ CH}_3 \text{COOH} + 1.14 \text{ O}_2$ $\rightarrow \textbf{0.43 N}_2 + 0.11 \text{ NO}_3^{-1} + 0.032 \text{ C}_5 \text{H}_7 \text{O}_2 \text{N} + \textbf{0.78 CO}_2 + 0.11 \text{ H}^+ + 1.26 \text{ H}_2 \text{O}$	

- N:
 - Full nitrification: ~96% N recovered as nitrate, ~81% C converted to CO₂
 - Partial nitritation/anammox:~86% N recovered as nitrogen gas, ~83% C converted to CO₂
- C:
 - For both: ~half of CO₂ production from urea; ~half of CO₂ production from COD
 - 17-19% of the incoming C is converted to biomass-C
 - **Assumptions:** Urine: ~1 g COD/g N → equivalent to ~0.22 mol acetic acid/mol N
 - Only aerobic COD conversion (no denitrification)
 - Aerobic COD conversion at 21-days mean cell retention time (sludge age)



Preliminary dimensioning and input/output assessment

- Volume nitrification or PN/A unit, assuming a loading rate of 0.5-1 g N/L/d (and a crew of 6):
 - 58-120 L active reactor volume
 - ca. 230-460 L reactor + skid/instrumentation/...
- Input/output:
 - Oxygen demand: Majority for N conversion
 - OH $^{-}$ demand: Only for full nitrification (\sim 1 mol OH $^{-}$ /mol N)
 - Sludge production: Similar for N and COD conversion
- Assumption: 9.6 g N/crew member/d in urine





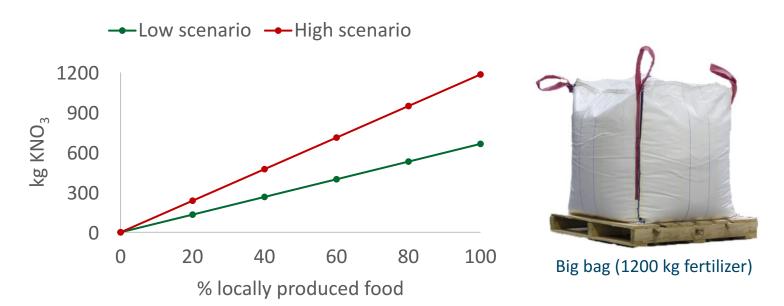
Enrique Peiro (and myself) at the MELiSSA Pilot Plant (UAB)

Note: sludge expressed in volatile suspended solids (VSS)



A thought exercise – Bring your N fertilizer from home

- Mission: 3 years, 6 astronauts
- Food production with 'conventional hydroponics': KNO₃ as N source, 14 ('low') -> 25 ('high') g N needed/person/day
- N fertilizer need: up to 660-1200 kg KNO₃
- Note: Not recycling water (12 L/person/day) requires about 79,000 kg H₂O -> 66-120x more mass





Nitrification-based urine treatment: The MELiSSA strategy towards demonstration in Space





Defined, axenic and always biosafe

-> 'curated/controlled' selection

Real: Full complexity (organics,

salts, micropollutants)

Reactor operation, modelling,

automation, control Fully integrated treatment

pipelines/systems

Reduced gravity (< 1 g)





Open, biodiverse and dynamic

-> 'natural/stochastic' selection

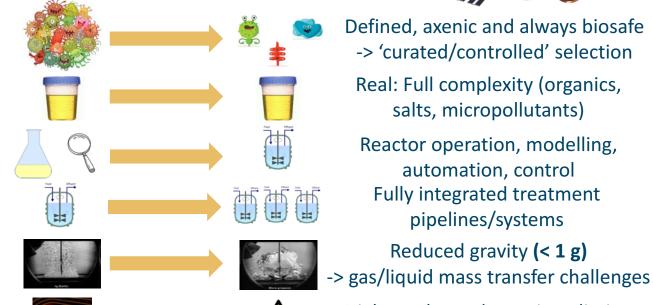
Synthetic: Progressively increasing complexity

Flask incubation and process characterization Storage, bioreactors and other unit processes

1 g

Radiation protected (magnetic field)

Ground demonstration









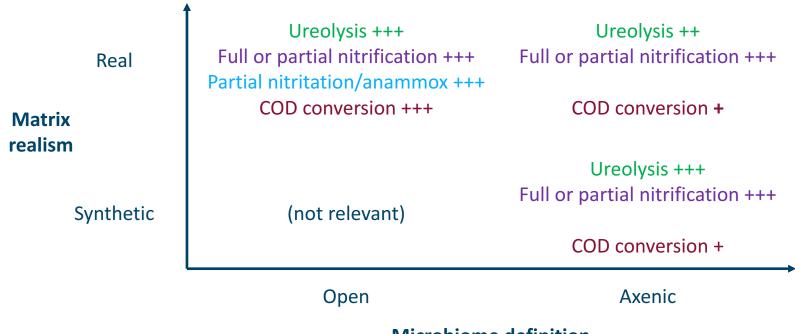
Higher solar and cosmic radiation

-> effects on biology (including crew) Space demonstration

+ Further system's decision making and optimization based on ALiSSE (advanced life support system evaluator) metrics: mass and energy requirements, reliability, and crew time and safety

Overview maturity microbiome and matrix types

- Development maturity with open communities > defined communities
- Development maturity N conversions > COD conversions
- To date, no 100% pure anammox cultures are available





Key achievements **open** communities

- Full nitrification (and COD conversion) demonstrated for undiluted urine (Coppens et al., 2016)
- pH control variations:
 - Full nitrification:
 - Alkalinization to stabilize in the collection/storage tank, at no surplus base 'cost' (a.o. De Paepe et al., 2018)
 - Chemical OH⁻ addition (a.o. Coppens et al., 2016)
 - Electrochemical OH⁻ addition (De Paepe et al., 2021)
 - Partial nitrification on 'spontaneously' fermented/ureolysed: pH-based feeding, no OHaddition (e.g. Faust et al., 2023)
- Particle-free effluent through use of membrane bioreactors (Coppens et al., 2016; De Paepe et al., 2018)
- First insights into N_2O emissions and optimization potential (0.4-1.2% of N load) (Faust et al., 2022a)
- Insights into understanding and avoiding ingrowth of novel acid-tolerant ammonia oxidizer
 "Candidatus Nitrosoacidococcus urinae" (Faust et al., 2022b)
- Gravity-independent (bubbleless) aeration: membrane-aerated biofilm reactor (MABR) on real urine
 - Nitrification (De Paepe et al., 2020b)
 - Partial nitritation/anammox (Timmer et al., 2024)



Microbiomes for nitrification-based treatment solutions

Nitrifiers in a defined/synthetic microbiome: Once upon a time (1989): MELiSSA technical note 1

$$\frac{\text{Nitritation}: \text{NH}_{4}^{+} + 1.5 \text{ O}_{2}}{\text{Nitrosomonas}} \rightarrow 2 \text{ H}^{+} + \text{H}_{2}\text{O} + \text{NO}_{2}^{-} + 58-81 \text{ kcal}}$$

$$\frac{\text{Nitrosomonas}}{\text{Nitrobacter}} \rightarrow \text{NO}_{3}^{-} + 15-21 \text{ kcal}$$

$$\frac{\text{Nitrobacter}}{\text{Nitrobacter}}$$

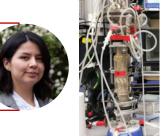
30+ years later -> Suitability confirmed for urine treatment:

- Nitrosomonas europaea
- Nitrobacter winogradskyi (e.g. Ilgrande et al., 2018)
- Anammox bacteria in an open microbiome: "Candidatus Brocadia sp." (in an open/mixed community; Timmer et al., 2024)



- Heterotrophs: The previously established consortium of four is currently being reconsidered (tested in UAB/MPP and UAntwerp): good for ureolysis, but limited for COD conversion
 - 1. Cupriavidus necator
 - **2.** Comamonas testosteroni
 - **3. Pseudomonas** fluorescens
 - **4. Acidovorax** delafieldii





Key achievements **defined** communities

With focus on the nitrifiers (Nitrosomonas and Nitrobacter):

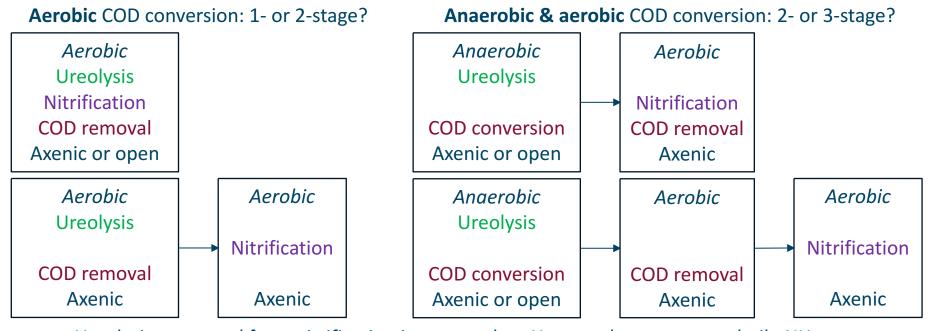
- Predictive modeling (Cruvellier et al., 2016)
- Very high nitrification rates: 1.7-2.5 g N/L/d (100-54% efficiency) (Cruvellier et al., 2017)
- Proteomic understanding of salt effects on nitrification (Ilgrande et al., 2018)
- Reactor operation demonstrated at the salinity of undiluted urine for nitrification (Christiaens et al., 2019)

With focus on the heterotrophic bacteria (ureolysis; COD conversion):

- Selection of ureolytic, salt-tolerant heterotrophs with batch tests (Ilgrande et al., 2018)
- First reactor treatment of real urine achieved with defined nitrifiers (Christiaens et al., 2019)
- First reactor treatment with real urine at **high nitrate production rates** (>0.5 g N/L/d) (Queralt Farras/Marcel Vilaplana/Carolina Arnau, MPP/UAB)



Best route to integrate conversion of urinary organics with nitrification?



- Ureolysis separated from nitrification increases the pH -> need to manage volatile NH₃
- Anaerobic pre-treatment (fermentation):
 - Yields volatile fatty acids (mainly acetic acid), which easing axenic aerobic conversion
 - Can replace the collection/storage tank and the alkalinization/stabilization
 - Can be integrated with organic waste treatment scenarios
- Axenic or (biosafe) open? Function of treatment/recovery goal and mission scenario



Key pipeline/integration/system achievements

- Pre-treatment:
 - Alkalinization: Electrochemical (De Paepe et al., 2020a) or chemical (a.o. De Paepe et al., 2018)
 - Spontaneous 'maturation': ureolysis (Udert et al., 2003) and organics fermentation (Eawag, POMP Nele Kirkerup)
 - COD removal: Bio-anodic (De Paepe et al., 2020b) or aerobic (Heusser et al., 2024)
- Co-treatment of **urine** and:
 - Black water, organic waste (BWTB, KULeuven)
 - Grey water (shower), condensate (Lindeboom et al., 2020)
- Post-treatment, valorization and integration:
 - Water recovery integrated process (Lindeboom et al., 2020)
 - Concentrated liquid fertilizer production (incl. removal of micropollutants and water)
 (Eawag/VUNA)
 - Food and oxygen production on urine with microalgae and plants (C4a and C4b) (UAB/MPP; CIRiS: Øyvind Jakobsen)
- System aspects
 - Automation and control (a.o. Sherpa Engineering; Université Clermont Auvergne)
 - Stochastic Space mission scenario analyses (Van Winckel et al., in prep.)
 - Preliminary establishment ALiSSE (advanced life support system evaluator) metrics
 - Terrestrial environmental sustainability assessment (Appiah-Twum et al., 2025)

Talks later in this session (2.2):

Øyvind Jakobsen:

15h45

Nele Kirkerup:

16h15





Nitrification-based processes in Space

Experiment	BiSTRO	Nitrimel
Research topic	Reactivation potential of stored microbes (executed)	
Conversions	Nitrification	Nitrification, ureolysis, denitrification, anammox
Activity determination	Pre- and post-flight batch reaction	Post-flight batch reaction

(Ilgrande (Lindeboom et al., 2019) et al., 2018)

MELiSSA's EC(R)LSS view on 'nitrification-based' urine treatment: Win-win-win-...

-> Nitrification-based processes modularly and flexibly fit in many EC(R)LSS goals/scenarios:

دے

1. Environmental control (EC) -> Waste treatment for risk mitigation



Vitrification-based conversion C3

CO,

Salts for food production

(P, K, Ca, Mg, S,...)

Regenerative life support systems (RLSS)

-> Resource recovery to increase circularity and decrease external dependency



biofouling, scaling, **3A.** Produce N₂ gas NO₂ (+ NH₄+)

organics)

biological oxygen demand,...

Avoid NH₃ volatilization,

for atmosphere provision

for biological nitrogen fixation for food/O₂ production

AND/OR 3B. Produce a mineral nutrient solution for food/O₂ production

For all goals, the processes are feasible for 'just' urine (+ condensate) but also any more complex waste treatment effluents or MELiSSA cycle (faeces +/- organic waste +/- grey water +/- ...)

What about MELiSSA-inspired nitrification solutions for Earth?



Tapping into human and animal urine?





Manneken Pis (1619)

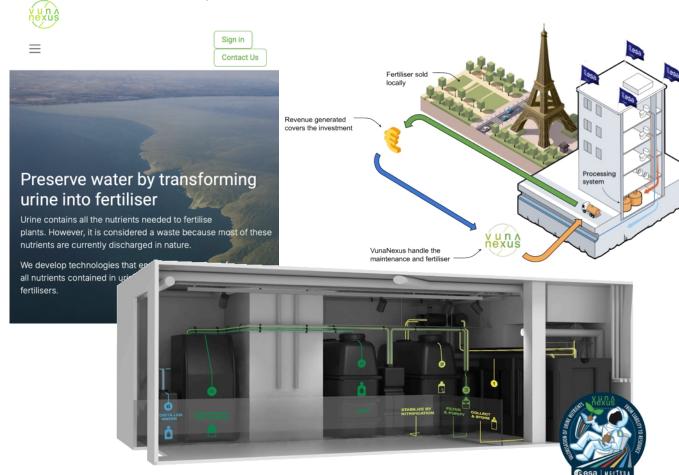


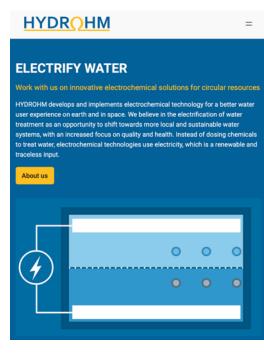
Jeanneke Pis (1987)



Zinneke Pis (1999)

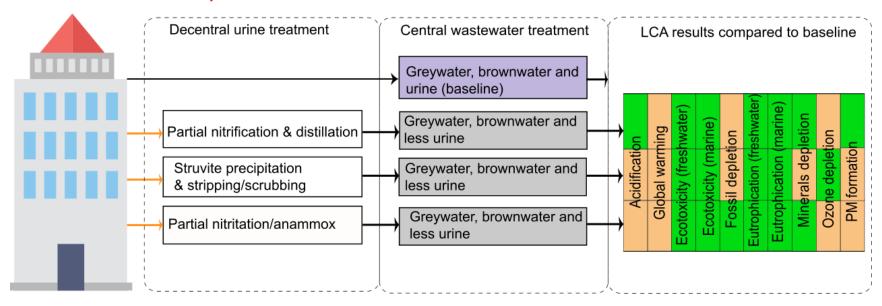
Companies for urine treatment solutions: Vuna Nexus & Hydrohm







Environmental impact **centralized <-> decentralized urine** collection and treatment



Hybrid scenarios showed increased impacts on global warming compared to the baseline

Hybrid scenarios performed better in 9 out of 10 categories.

Legend

- Hybrid scenarios have a lower global warming impact at higher central WWTP N₂O emissions and electricity use
- Urine alkalinization showed a higher impact in 7 out of 10 categories (Appiah-Twum et al., 2025, Water Research)

Lower impact than the baseline

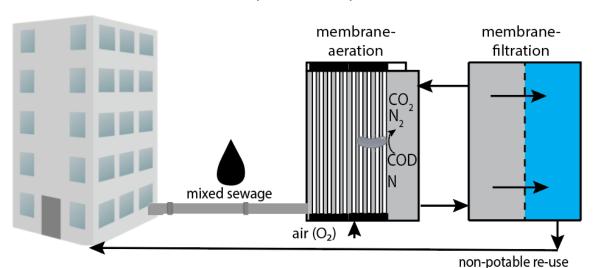


Higher impact than the baseline

Hanson Appiah-Twum



TwinMemBio: COD and N removal in a membrane-aerated membrane bioreactor (MA-MBR) for resource-efficient local water reuse



Marijn Timmer

Compared to conventional bubble-aerated MBR (BA-MBR):

- Energy savings
- Space savings

- **V**
 - Successful 1-stage simultaneous nitrification/denitrification
- ✓ St
 - Stable treatment sewage with COD/N ratio 5-20
- **√**
- Oxygen demand (=TN+COD) loading rates of > 4 g O_2 L⁻¹ d⁻¹ vs. 2 in bubble-aerated MBR
- Effluent quality adheres to strictest domestic re-use standards COD, BOD_5 , NH_4^+ and TN







Lowering nitrogen emissions from dairy farms: Treating cow urine



CowToilet (Hanskamp)



- Simple and robust biofilm reactor technology: Rotating biological contactor (RBC)
- Cow urine:
 - Relatively high COD/N (~5); N ~ 4 g N/L (undiluted)
 - Partially ureolyzed, despite source separation
- Pre-treatment: Alkalinization <-> Acidification
- Operation at ~33% and ~50% urine:
 - pH ~7.4; EC ~30 mS/cm
 - High N and COD removal efficiencies (>90%)
 - Removal rates around 100 mg N/L/d and 500 mg COD/L/d (20°C)
- Next step: transition to undiluted cow urine





Patricia Gutierrez

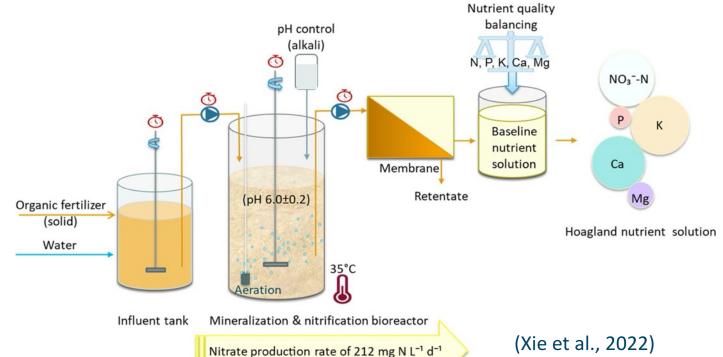


Iris De Corte



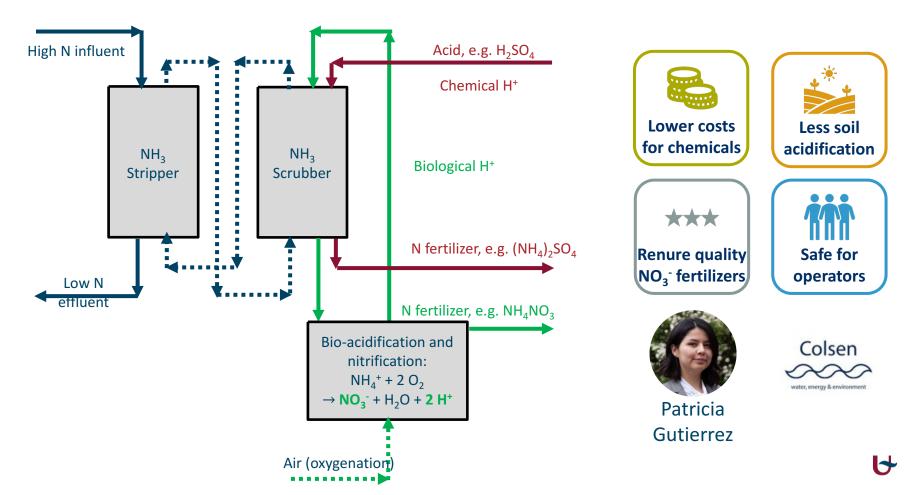
Transforming solid organic fertilisers to nitrate-based liquid fertiliser solutions for horticulture

- Mineralized and nitrification of solid organic fertilizers in an aerobic bioreactor
- pH control with Ca(OH)₂ or Mg(OH)₂ supplements plant macronutrients
- Besides recovered nutrients in solution, also CO₂ can be used for plant production
- The concept has the potential to be economically feasible for hydroponics





The **BioCatcher** concept: A bioscrubber overcoming the challenges of chemical acid scrubbing



























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Marc Spiller, Tim Van Winckel,

Jolien De Paepe, ...





Ramon Ganigué, Nico Boon, Peter Clauwaert, Korneel Rabaey,

Ralph Lindeboom, Jolien De Paepe, Celia Alvarez Fernandez,...





Ilse Smets, Koen Rummens....





















Universitat Autònoma de Barcelona





Faust, Philipp Markus, Nele Kirkerup,...







vision on technology

Francesco Gòdia, Enrique Peiro, Carolina Arnau, Queralt Farràs Costa, David García, Carles Ciurans, Justyna Barys, Marcel

SEMILLA IPSTAR Circular Systems™

Rob Suters, Radu Giurgiu,...

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Baptiste Leroy, Ruddy Wattiez, Neha Sachdeva, Thanh Huy Nguyen,...

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