



CREATING  
A CIRCULAR  
**FUTURE**

# MELISSA Pilot Plant Status and Perspective

Francesc Gòdia

MELISSA Pilot Plant – Claude Chipaux Laboratory

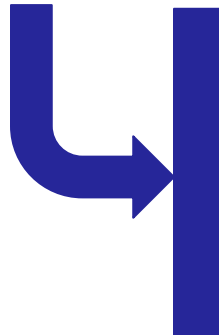
Universitat Autònoma de Barcelona



# Main requirements for Human Space Exploration and life support systems.



## Human Space Exploration: main challenges



Safety and protection for the crew. Radiation

Advanced Propulsion. Reduction of mission time

Life support. Make the mission possible

Air revitalization

Water reutilization

Waste management

Food production and preparation

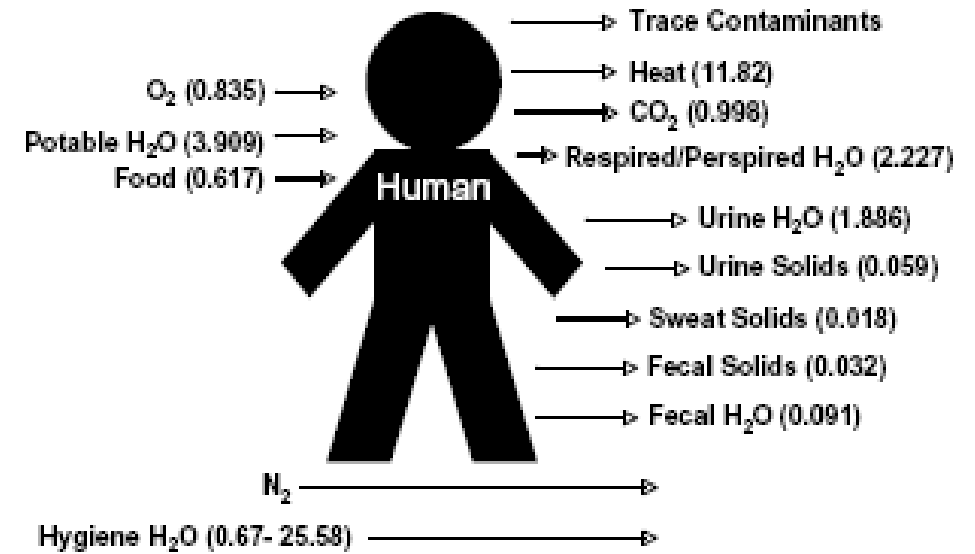


Figure 1. Human Consumable and Throughput Values in kg (or MJ)/crewmember/day

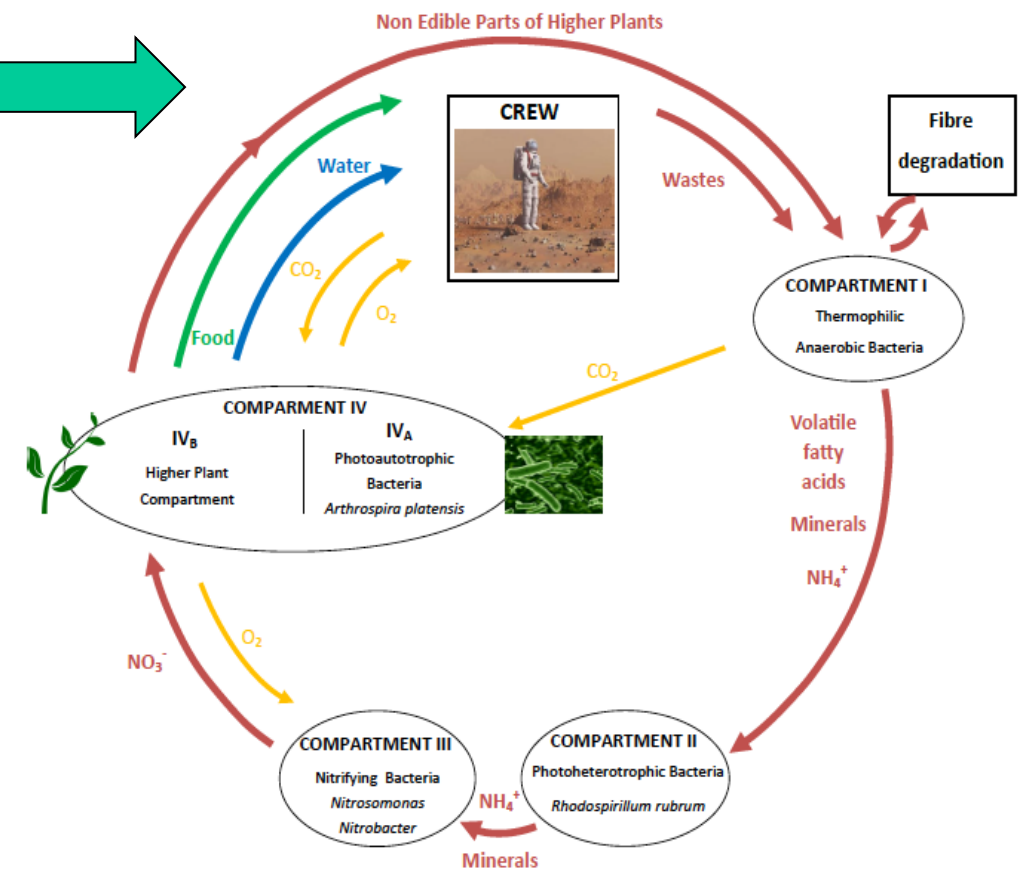
Metabolic consumables: 5 kg/day/person, 6 crew members, 1000 days: 30.000 kg (without hygiene water)  
Best launchers could only drop 9 tones ... **long-term missions need regenerative LSS**



# The MELiSSA Concept



MELiSSA approach is to perform the most relevant biological functions of an ecosystem in individual compartments (bioreactors and higher plant chambers), in continuous and controlled operation



# The MELiSSA Pilot Plant



## Main objectives

Integration and demonstration of the MELiSSA concept at pilot scale

Technology demonstration:

In ground conditions

With an animal crew

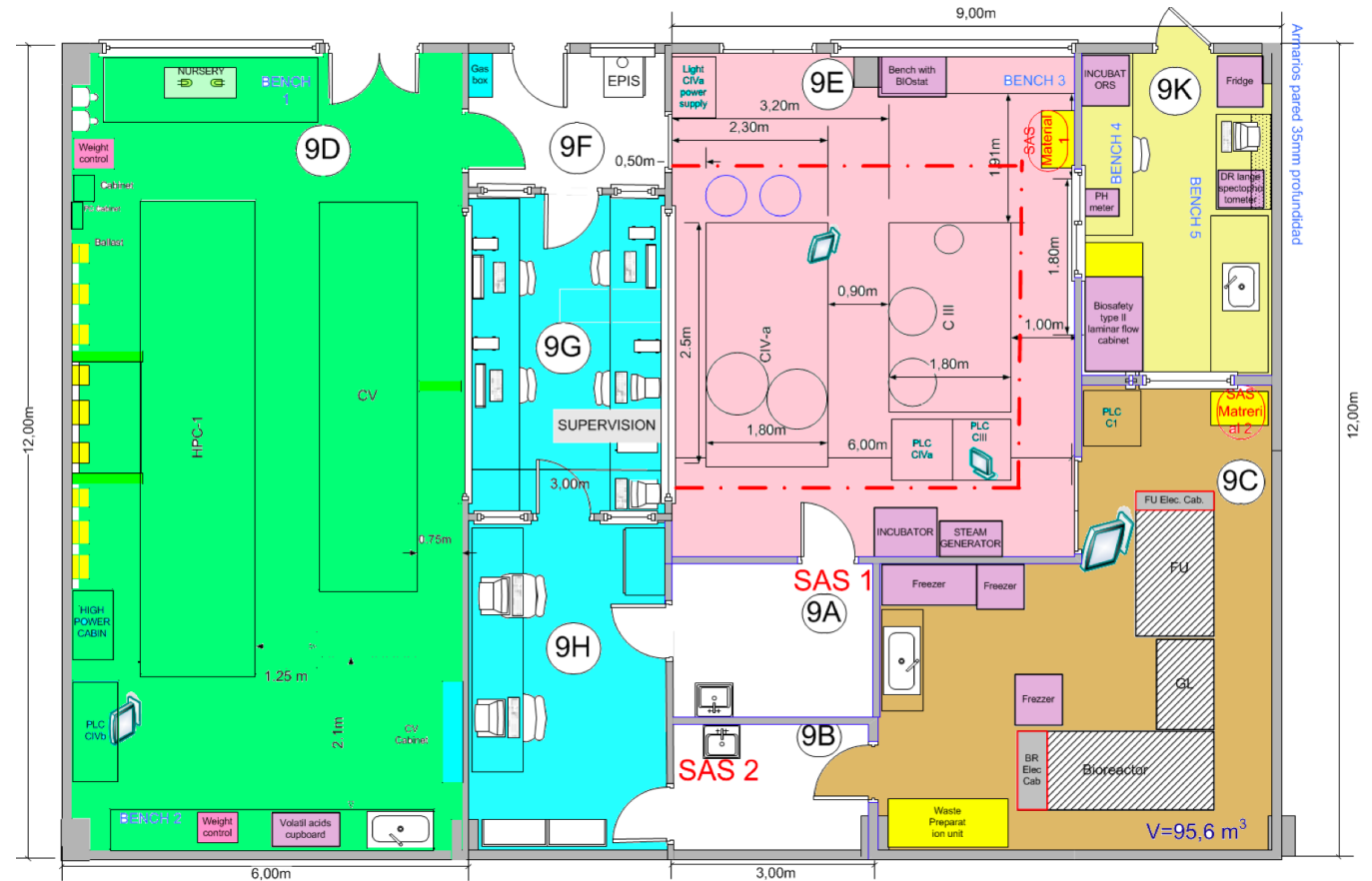
With industry standards

Long-term continuous operation

Modelling and Control

Production of Oxygen: equivalent to a one person respiration  
 Production of food: at least 20% of a person requirements

## Layout (214 m<sup>2</sup>)



**Comp. IVb and CV**

**Comp. III and IVa**

**Control and supervision**

**Comp I**

**Analysis Laboratory**

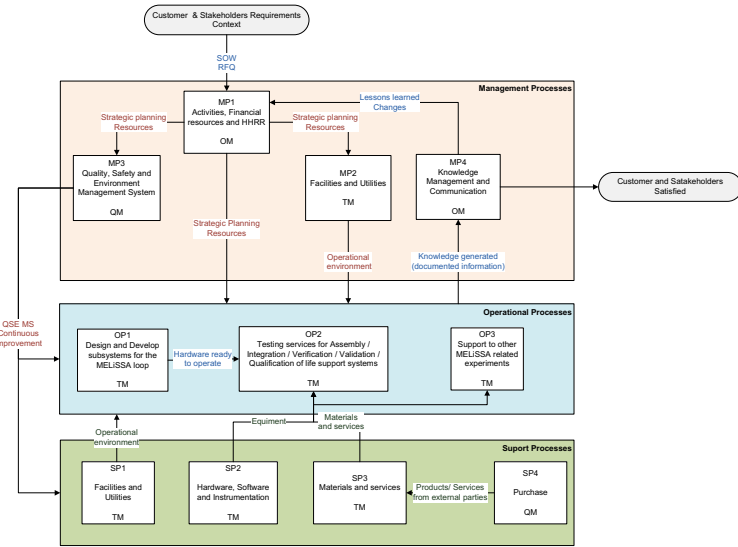


# The MELiSSA Pilot Plant: Clean room up-grade





# Quality and Systems Engineering approach as working framework



ZERTIFIKAT ♦ CERTIFICATE ♦ CERTIFICADO ♦ CERTIFICAT

## CERTIFICATE

The Certification Body of TÜV SÜD Management Service GmbH certifies that

**the MELISSA Pilot Plant – Claude Chippaux Laboratory (MPP-CCL)**  
the European Space Agency external facility for life support systems ground demonstration, located at  
Dpto. Ingeniería Química, Escola d'Enginyeria, Universitat Autònoma de Barcelona  
E-08193 Bellaterra

has established and applies a Quality Management System for

Life support systems ground demonstration consisting of the three following operational processes:

- OP1 - Design and develop hardware subsystems for the MELISSA loop
- OP2 - Provide leading services for assembly/integration/verification/validation/qualification of its support subsystems
- OP3 - Provide support to other MELISSA related experiments.

An audit was performed, Report No. 7079265  
Proof has been furnished that the requirements according to

**ISO 9001:2008**  
are fulfilled. The certificate is valid until 2014-07-31  
Certificate Registration No. 12 100 42856 TMS

*M. López*  
München, 2012-05-08  
089-789-28-0140  
TÜV SÜD Management Service GmbH • Zertifizierungsbüro • Rinderstraße 91 • 80329 München • Germany • TÜV

**MELISSA Pilot Plant**  
UAB  
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**QUALITY ASSURANCE PROCEDURE**

Document Identification	Code	Issue	Page
FACILITIES QUALIFICATION, CLEANING AND CONTAMINATION CONTROL PROGRAM	MPP-QAP-08-007	(1)	1 / 15

MPP-13/MPP-15-QAP-08

**MELISSA Pilot Plant**  
Quality Assurance Procedure for  
Facilities qualification, cleaning  
and contamination control program

Prepared by (visa): Beatriz Irigoin Date: 11/01/16 Quality Manager	Checked by (visa): Enrique Peiro Date: 11/01/16 Technical Manager	Approved by (visa): Francesc Gòdia Date: 11/01/16 Overall Manager	Quality Manager: Beatriz Irigoin Date: 11/01/16
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Approved by (visa): Brigitte Lamaze Date: 11/01/16 ESA Focal Point for MPP	Release date: 11/01/16 in case equal per insurance bond	Expiry date: 11/01/16 in case equal per insurance bond
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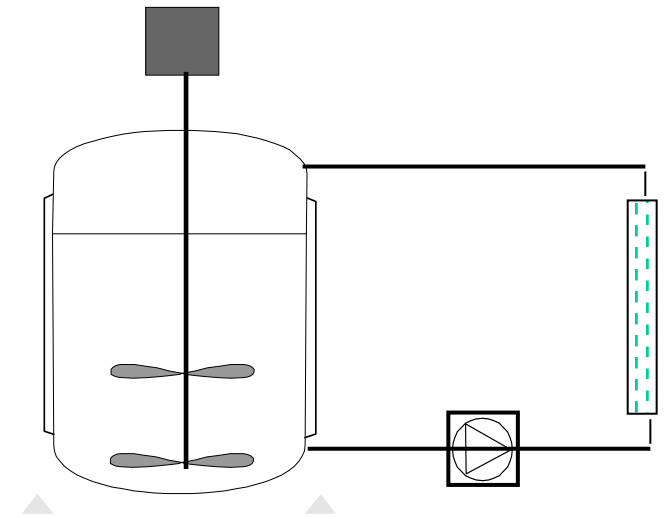
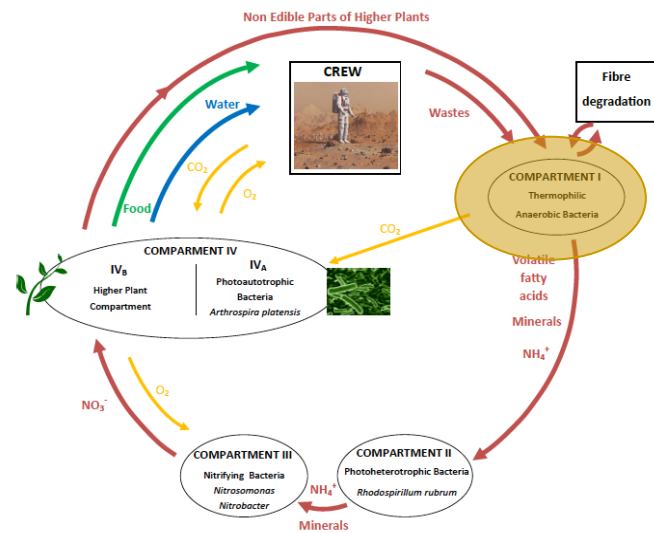
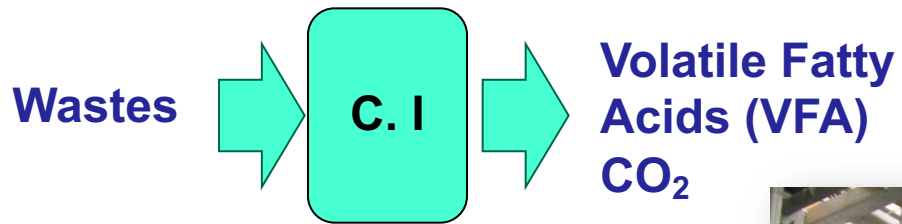
# Compartment I



Waste recovery

Mixed thermophilic anaerobic bacteria

Stirred tank

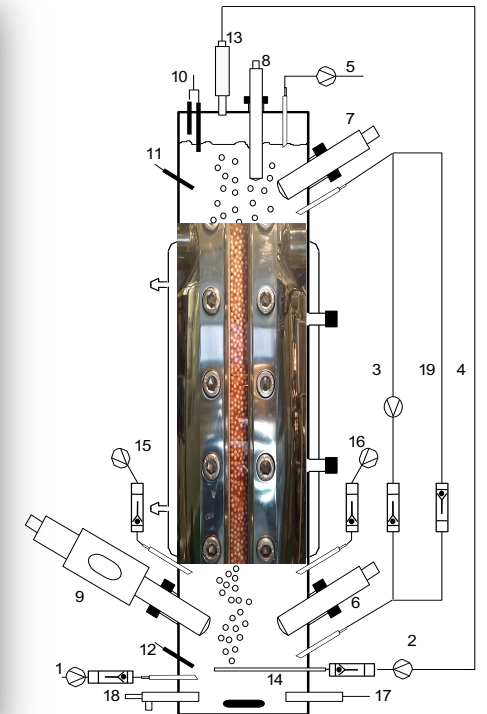
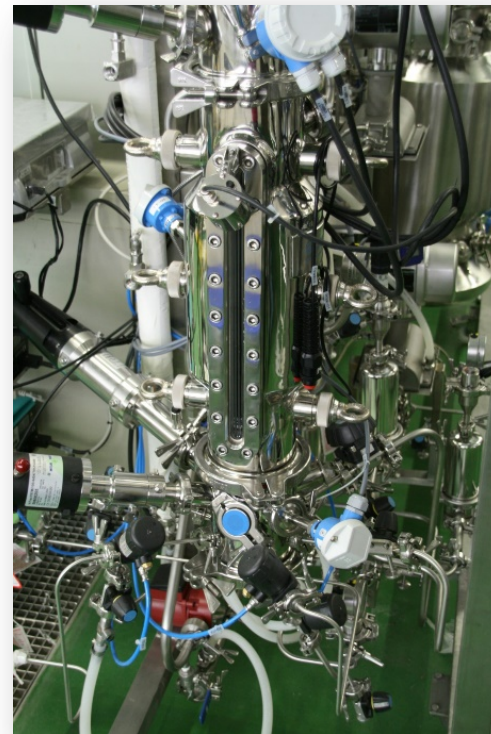
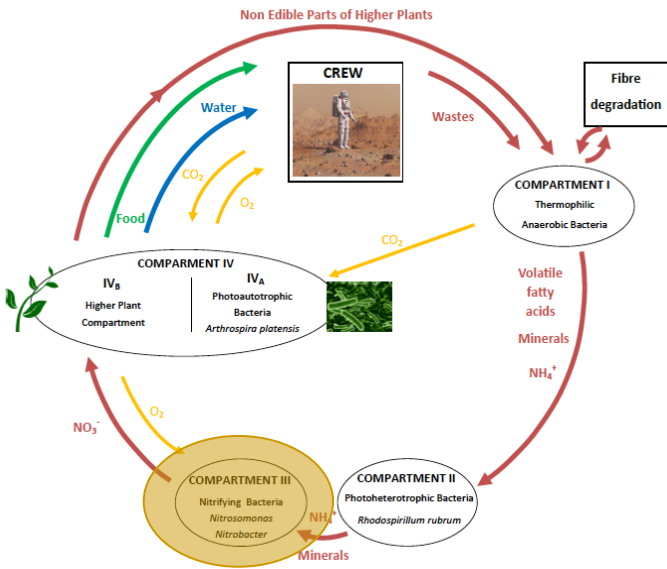
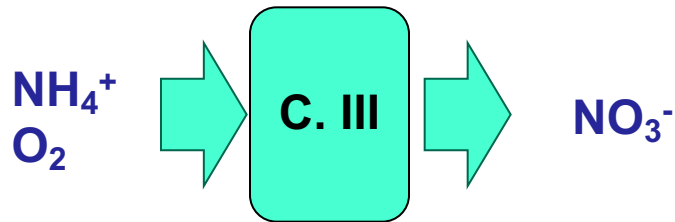


# Compartment III

## Nitrification

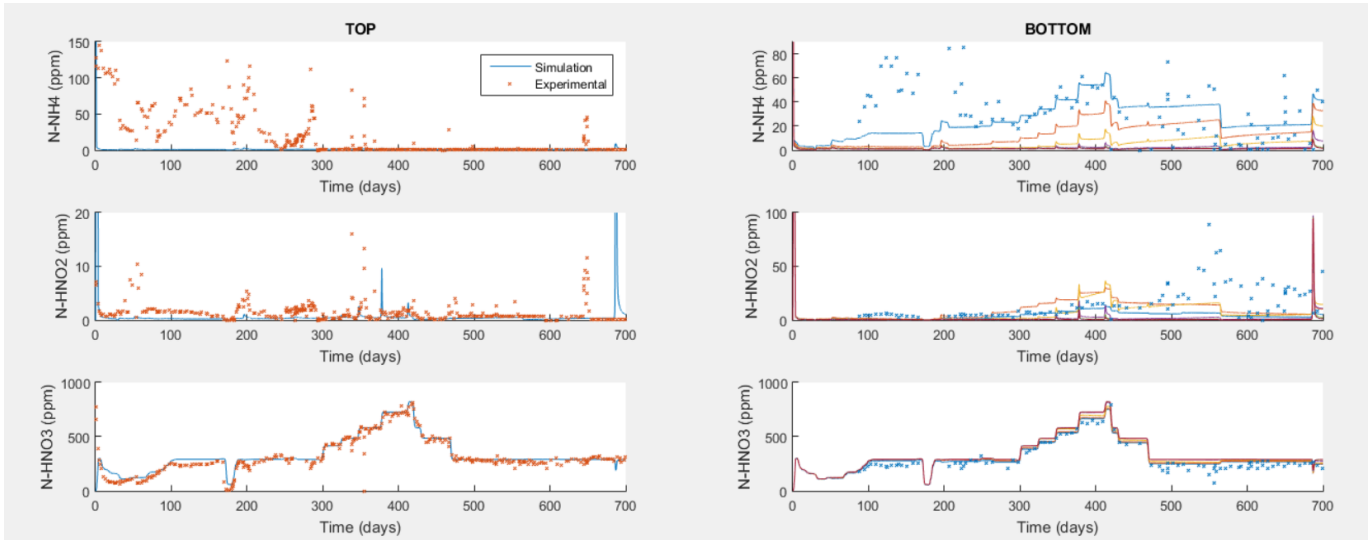
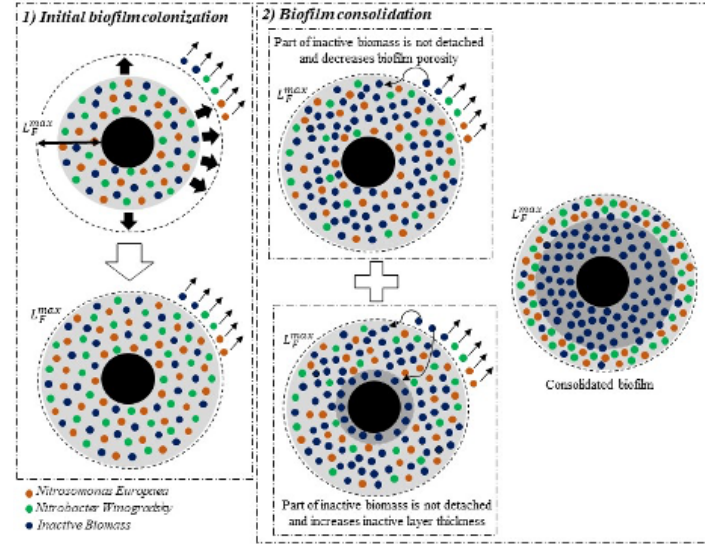
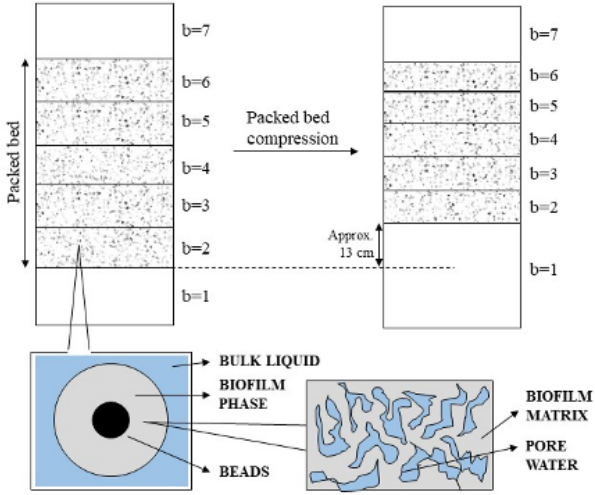
## *Nitrosomonas europaea* and *Nitrobacter winogradsky* (axenic co-culture, aerobic)

## Packed-bed bioreactor





# Compartment III: modelling (L. Alemany, modelling session)



$$\dot{C}_{\ell,j}^{[b]} = \frac{1}{V_\ell^{[b]}} \left( \dot{M}_{\ell,C_{\ell,j}}^{in[b]} - \dot{M}_{\ell,C_{\ell,j}}^{out[b]} + \sum_{i=1}^{n_x} \left( Y_{j/i} + Y_{j/i}^m \frac{m_i}{\mu_{max,i}} \right) (R_{\ell,X_i}^{[b]} + R_{F,X_i}^{[b]}) \right)$$

$$\dot{X}_{\ell,i}^{[b]} = \frac{1}{V_\ell^{[b]}} \left( \dot{M}_{\ell,X_{\ell,i}}^{in[b]} - \dot{M}_{\ell,X_{\ell,i}}^{out[b]} + R_{\ell,X_i}^{[b]} + u_{det}^{[b]} A_F^{[b]} \bar{X}_{F,i}^{[b]} \right) - b_i^{lethal} X_{\ell,i}^{[b]}$$

$$\dot{X}_{\ell,0}^{[b]} = \frac{1}{V_\ell^{[b]}} \left( \dot{M}_{\ell,X_{\ell,0}}^{in[b]} - \dot{M}_{\ell,X_{\ell,0}}^{out[b]} + u_{det,0}^{[b]} A_F^{[b]} \rho_{bio} (1 - \varepsilon_{F,\ell}^{[b]}) \varphi_{F,0}^{[b]} \right) + \sum_{i=1}^{n_x} b_i^{lethal} X_{\ell,i}^{[b]}$$

$$\dot{C}_{g,j}^{[b]} = \frac{1}{V_g^{[b]}} \left( \dot{M}_{C_{g,j}}^{in[b]} - \dot{M}_{C_{g,j}}^{out[b]} + k_{LA,j} (C_{\ell,j}^{[b]} - C_{\ell,j}^{*[b]}) V_\ell^{[b]} \right)$$

$$\dot{X}_{F,i}^{[b]} = \frac{R_{F,X_i}^{[b]}}{V_F^{[b]}} - \frac{u_{det}^{[b]} A_F^{[b]}}{V_F^{[b]}} \bar{X}_{F,i}^{[b]} - b_i^{lethal} \bar{X}_{F,i}^{[b]} - \bar{X}_{F,i}^{[b]} \frac{\dot{V}_F^{[b]}}{V_F^{[b]}}$$

$$\dot{X}_{F,0}^{[b]} = - \frac{u_{det,0}^{[b]} A_F^{[b]}}{V_F^{[b]}} \bar{X}_{F,0}^{[b]} \times \frac{1000 L}{1 m^3} + \sum_{i=1}^{n_x} b_i^{lethal} \bar{X}_{F,i}^{[b]} - \bar{X}_{F,0}^{[b]} \frac{\dot{V}_F^{[b]}}{V_F^{[b]}}$$

$$\dot{L}_F^{[b]} = u_F^{[b]} - u_{det}^{[b]}$$

$$\dot{L}_{F,0}^{[b]} = \left( u_{att,0}^{[b]} - \phi_{F,0}^{[b]} \frac{A_F^{[b]}}{A_{F,0}^{[b]}} (u_{det}^{[b]} - u_{det,0}^{[b]}) \right) \frac{\bar{X}_{F,0}^{[b]}}{\rho_{bio} (1 - \varepsilon_{F,\ell}^{[b]})} - \left( \frac{A_{F,0}^{[b]} - A_b^{[b]} - \phi_{F,0}^{[b]} (A_F^{[b]} - A_b^{[b]})}{A_{F,0}^{[b]}} \right) \frac{\dot{L}^{[b]}}{2}$$

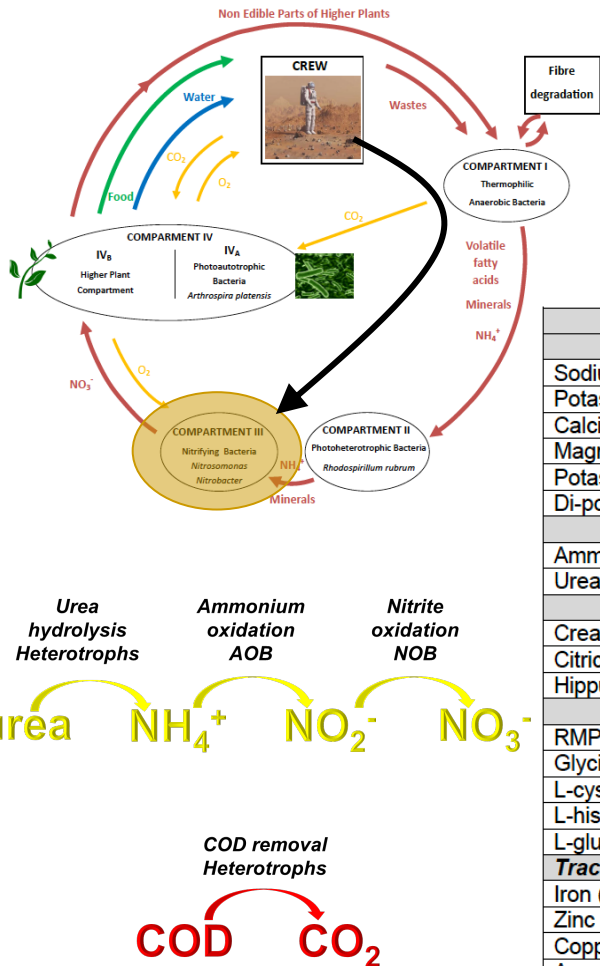
$$\dot{\varepsilon}_{F,\ell}^{[b]} = - \frac{1 - \varepsilon_{F,\ell}^{[b]}}{V_F^{[b]}} \left[ A_F^{[b]} (u_{det}^{[b]} - u_{det,0}^{[b]}) \varphi_{F,0}^{[b]} - (A_F^{[b]} - A_b^{[b]}) \frac{\dot{L}^{[b]}}{2} \right]$$

$$\dot{\eta}_\ell^{[b]} = - \frac{\dot{V}_b^{[b]} + \dot{V}_F^{[b]}}{V_T^{[b]}} + (1 - \eta_\ell^{[b]}) \frac{\dot{V}_T^{[b]}}{V_T^{[b]}}$$

$$\Delta \left\{ \dot{h}^{[b]} = \delta^{[b]} K (\eta_\ell^{[b]} - \eta_\ell^{min})^2 \frac{Q_{\ell,in} + Q_{\ell,recy}}{\frac{\pi}{4} D^2} \quad b = 2 \dots n - 1 \right\}$$

# Compartment III: preparing transition to urine

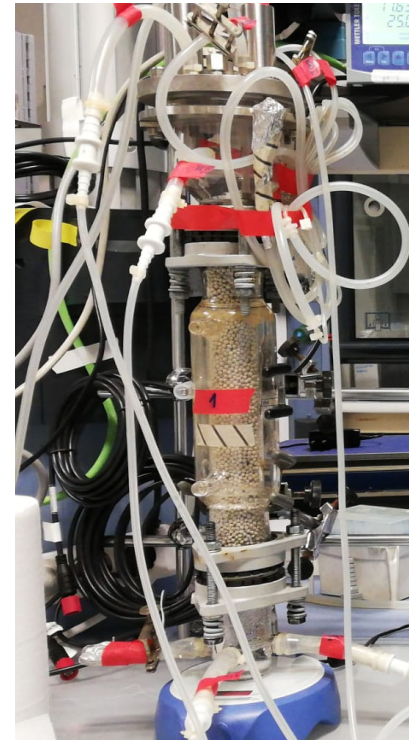
(M. Vilaplana, poster session)



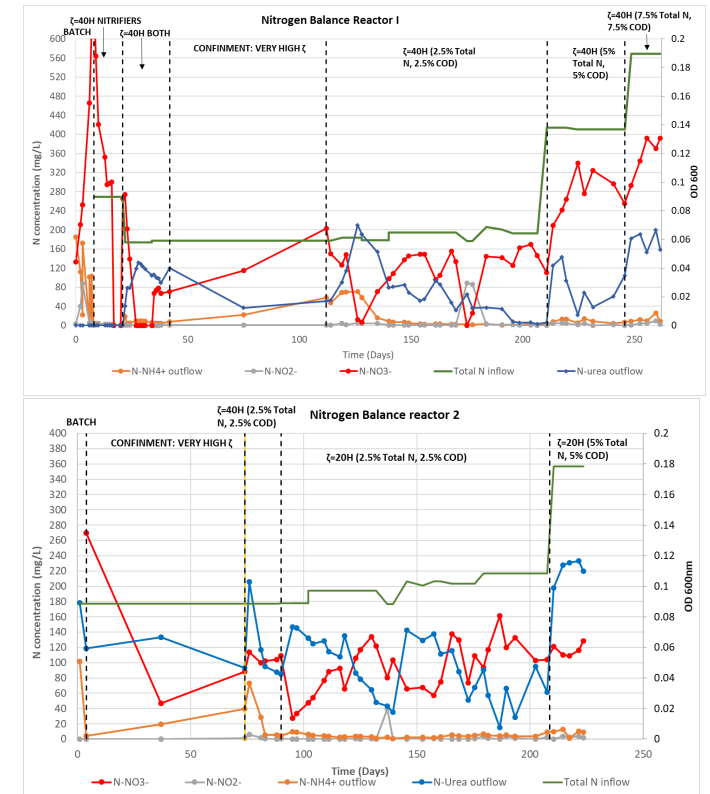
*Nitrosomonas europaea*  
*Nitrobacter winogradskyi*

**Synthetic urine**

Component	Concentration [g/L]
<b>Salts</b>	
Sodium chloride	0.500
Potassium chloride	0.100
Calcium chloride dihydrate	0.069
Magnesium sulphate heptahydrate	0.105
Potassium dihydrogen phosphate	0.190
Di-potassium hydrogen phosphate	0.240
<b>Nitrogen compounds</b>	
Ammonium sulphate	0.217
Urea	1.400
<b>Organics</b>	
Creatinine	0.469
Citric acid	0.162
Hippuric acid	0.170
<b>Amino acids</b>	
RMPI 1640 amino acid solution (50*)	2.5 ml/L
Glycine	0.032
L-cysteine	0.033
L-histidine	0.026
L-glutamine	0.023
<b>Trace elements</b>	
<b>Concentration [µg/L]</b>	
Iron (II) sulphate heptahydrate	50
Zinc sulphate heptahydrate	31
Copper (II) chloride dihydrate	27
Ammonium heptamolybdate tetrahydrate	77
Nickel (II) sulphate hexahydrate	22
Aluminium potassium sulphate	70



*Pseudomonas fluorescens*  
*Comamonas testosteroni*  
*Acidovorax delafieldii*  
*Cupriavidus necator*

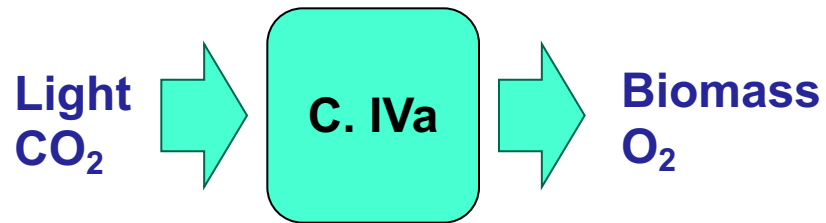




# Compartment IVa

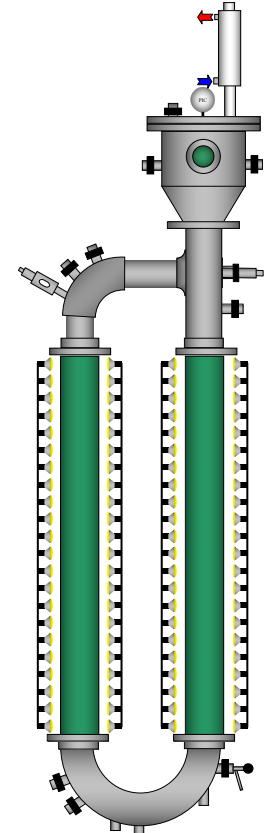
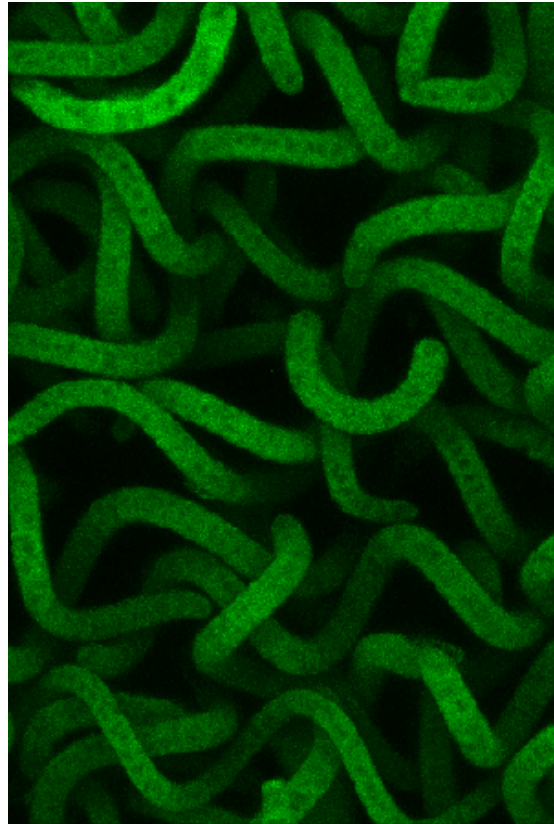
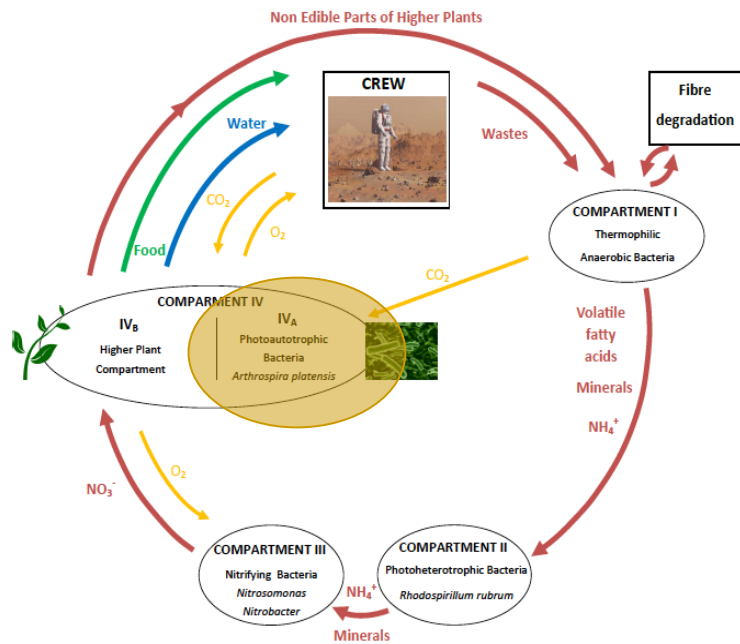


## Oxygen and Food production

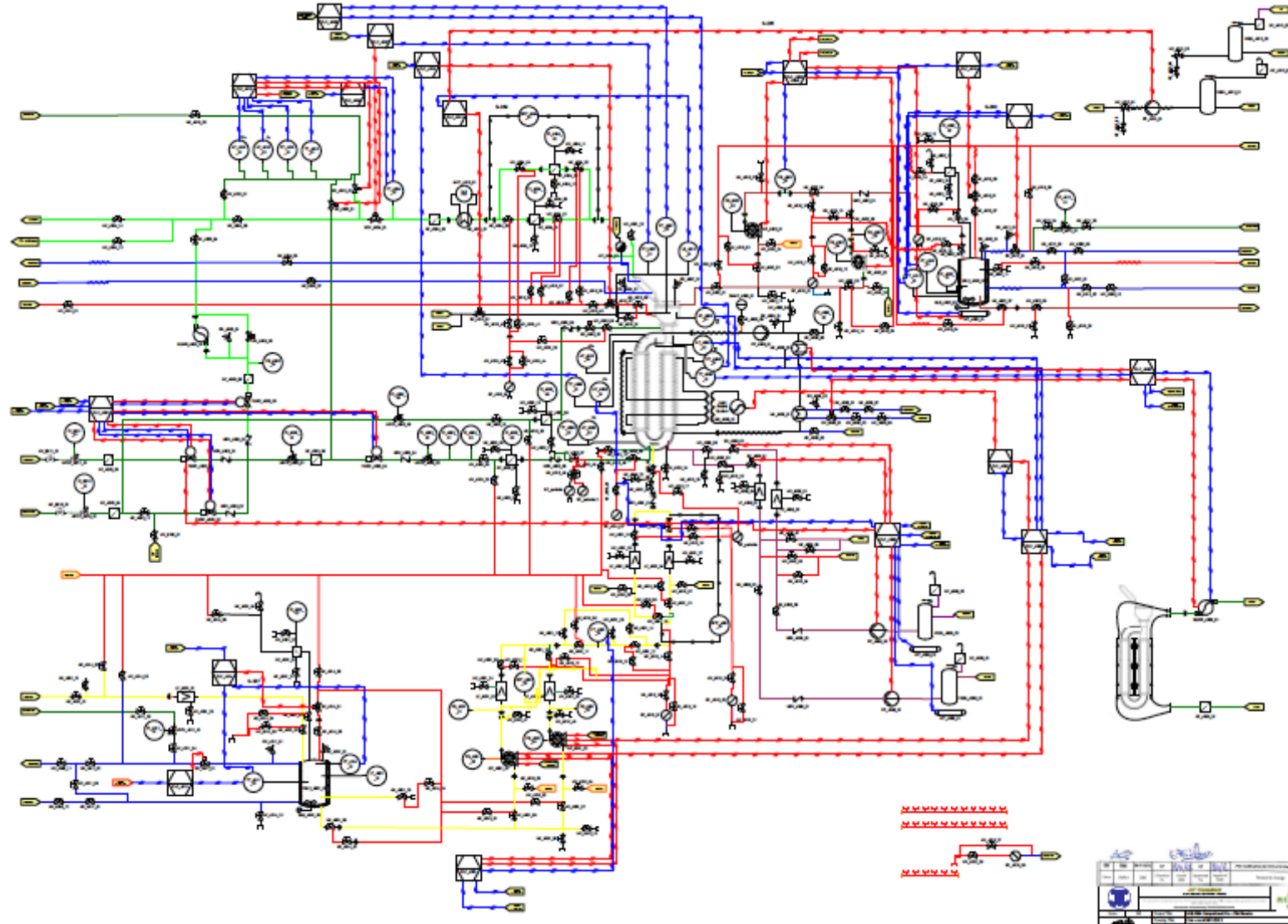


## *Limnospira indica*, also known as *Arthrospira platensis* (axenic culture)

## Photobioreactor

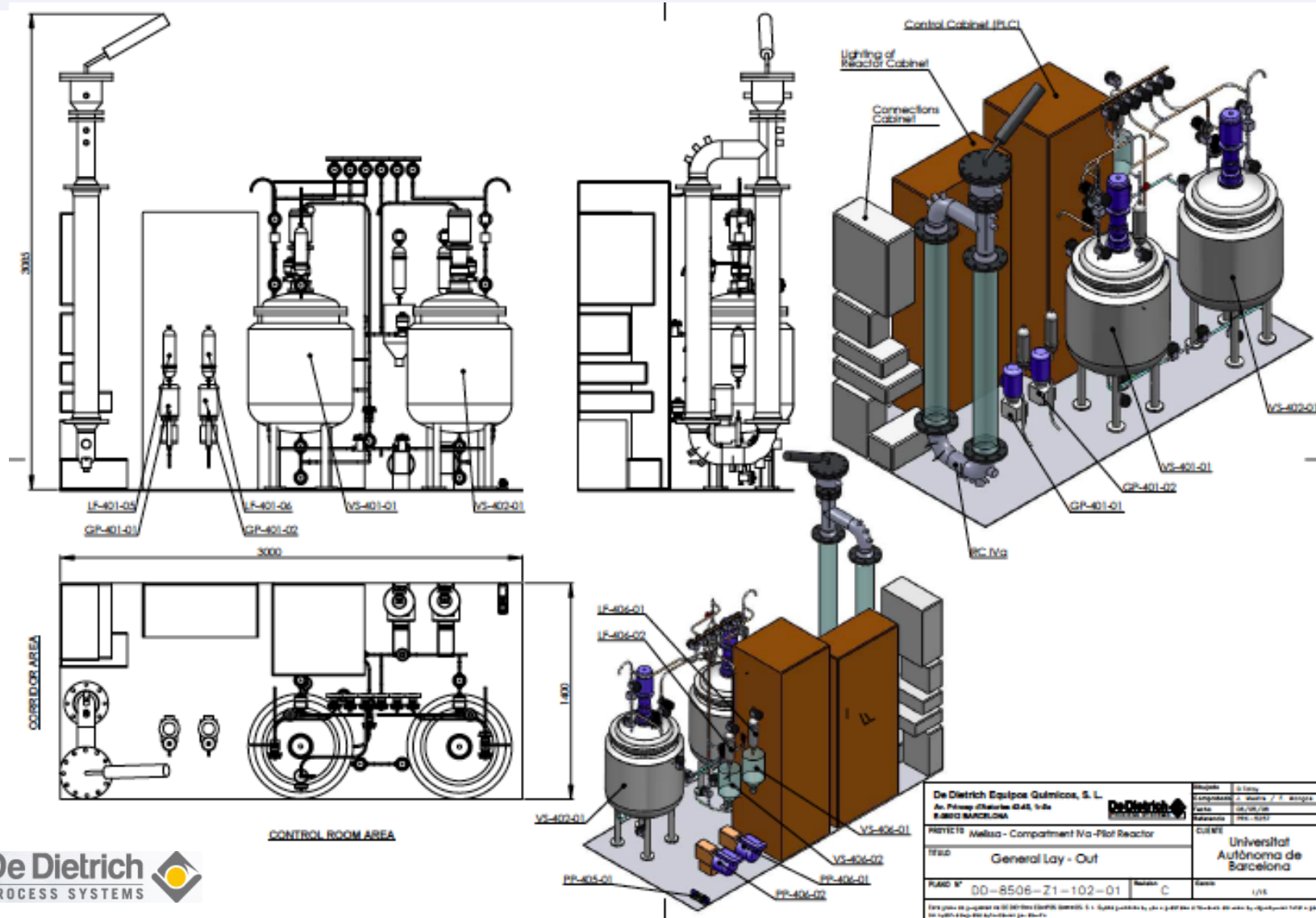


# Compartment IVa

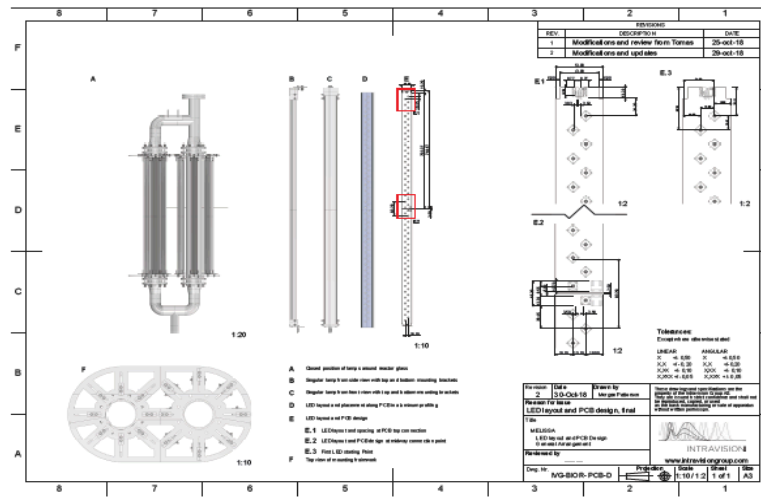
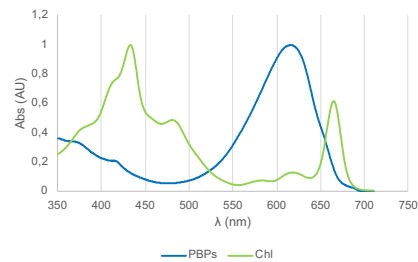
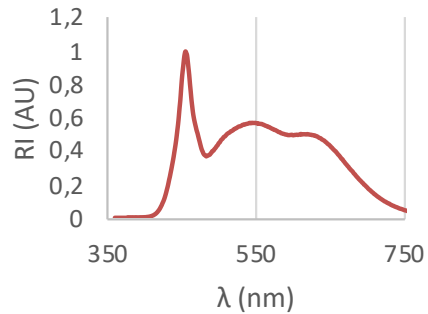
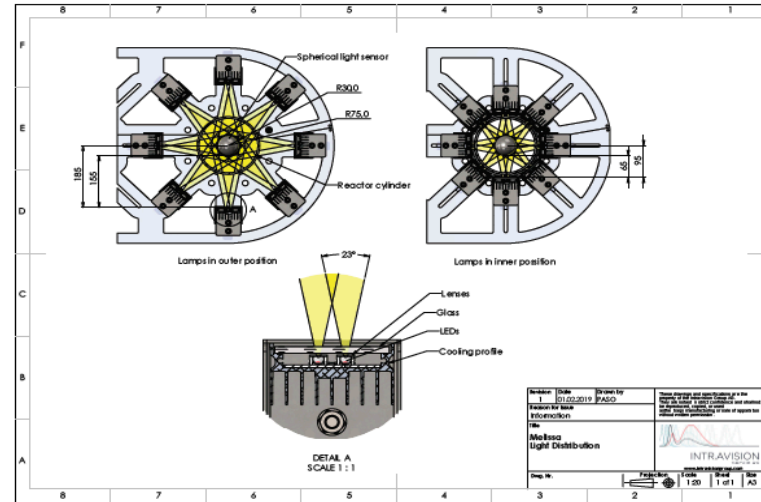




# Compartment IVa

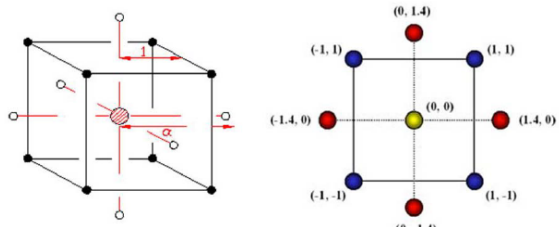


# Compartment IVa: new illumination system



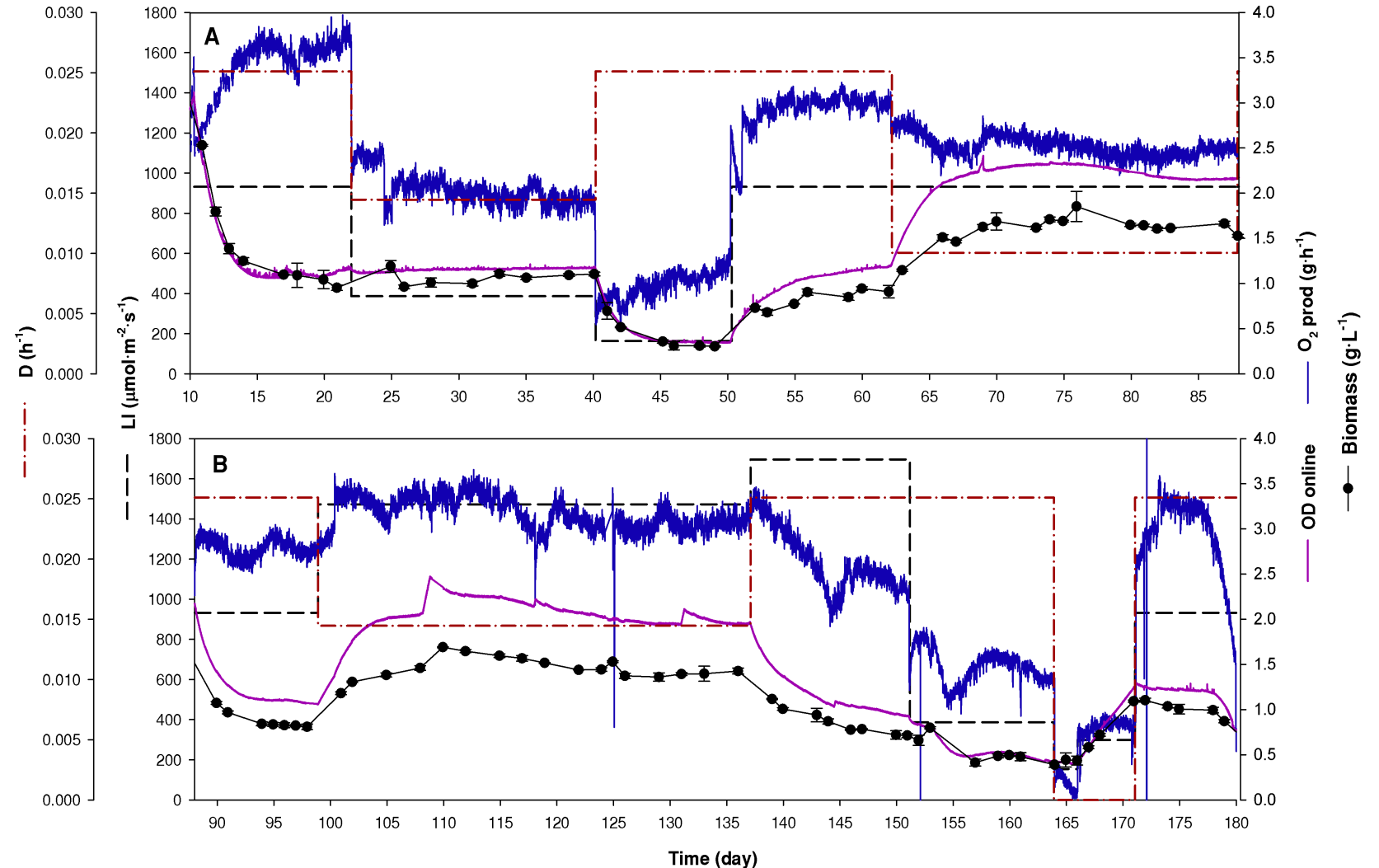


# Compartment IVb: new illumination system (D. García, microalgae and photobioreactors session)



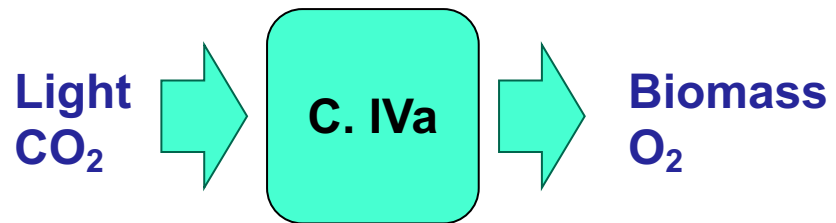
$$Y_n = b_0 + \underbrace{\sum_{i=1}^k b_i X_i}_{\text{Lineal}} + \underbrace{\sum_{i=1}^k b_{ii} X_i^2}_{\text{Curvature}} + \underbrace{\sum_{i=1}^k \sum_{j=1}^k b_{ij} X_i X_j}_{\text{Interaction}}$$

Exp	x1	x2	Q (L/h)	LI (%)
1	-1	-1	28.79	19.17
2	1	-1	71.21	19.17
3	-1	1	28.79	86.13
4	1	1	71.21	86.13
5	1.41	0	80.00	52.65
6	-1.41	0	20.00	52.65
7	0	1.41	50.00	100.00
8	0	-1.41	50.00	5.30
9	0	0	50.00	52.65
10	0	0	50.00	52.65
11	0	0	50.00	52.65
12	0	0	50.00	52.65
13	0	0	50.00	52.65

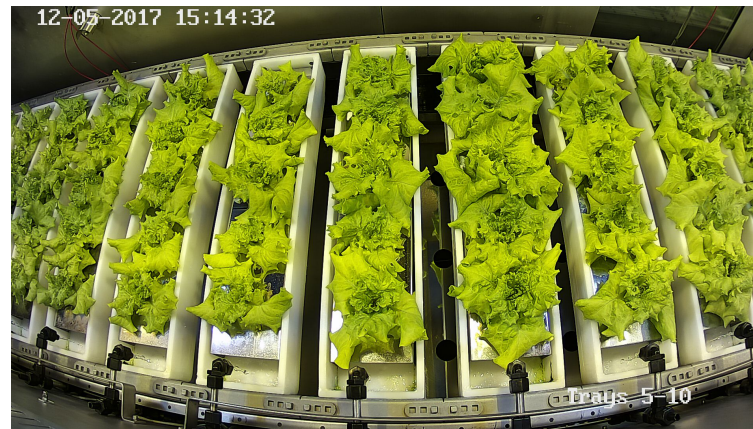
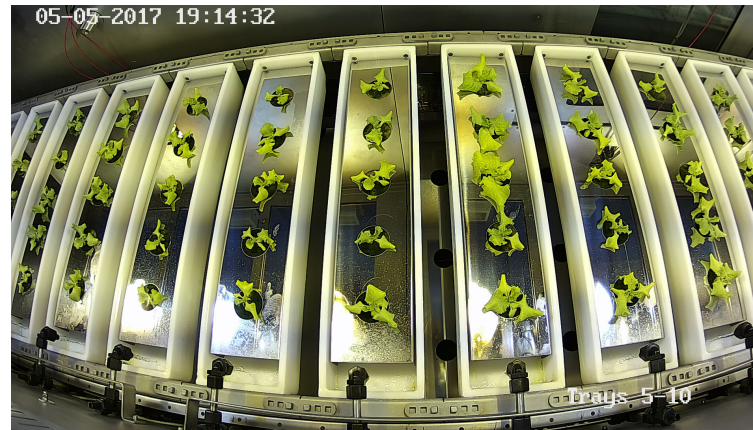


# Compartment IVb

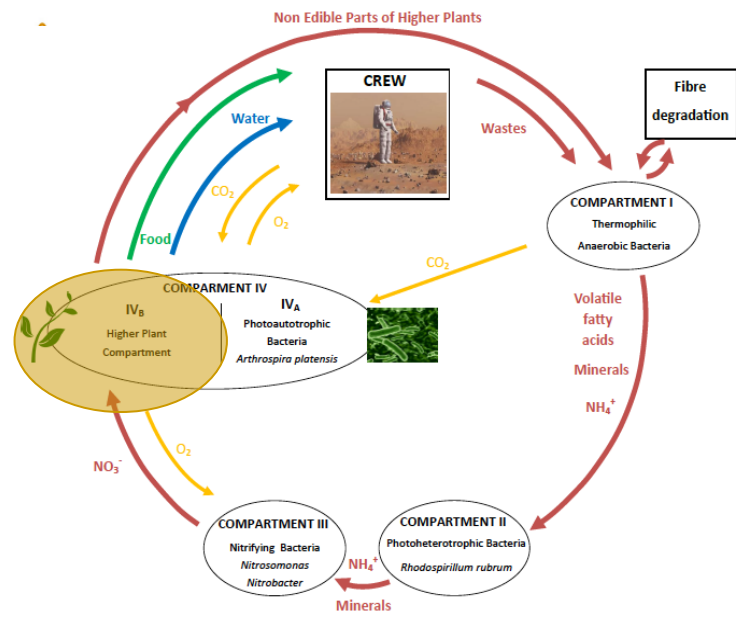
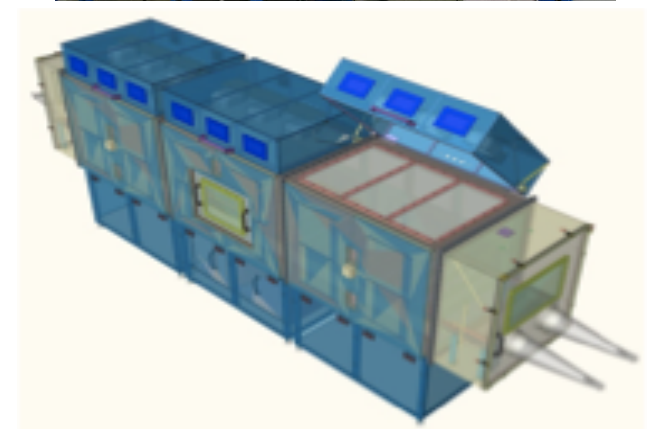
## Oxygen and Food production



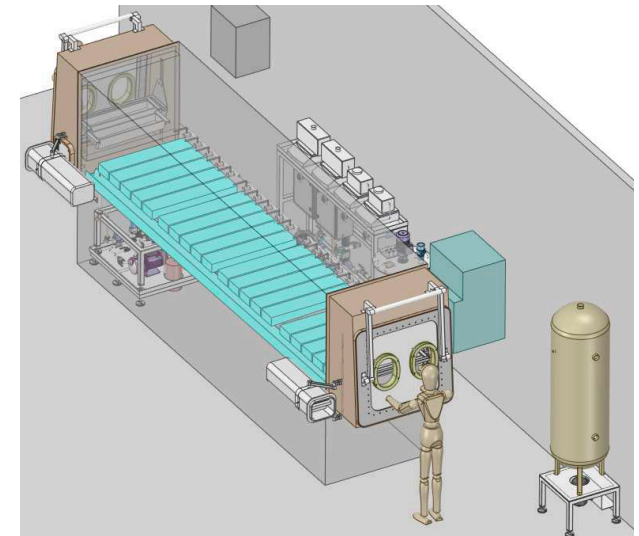
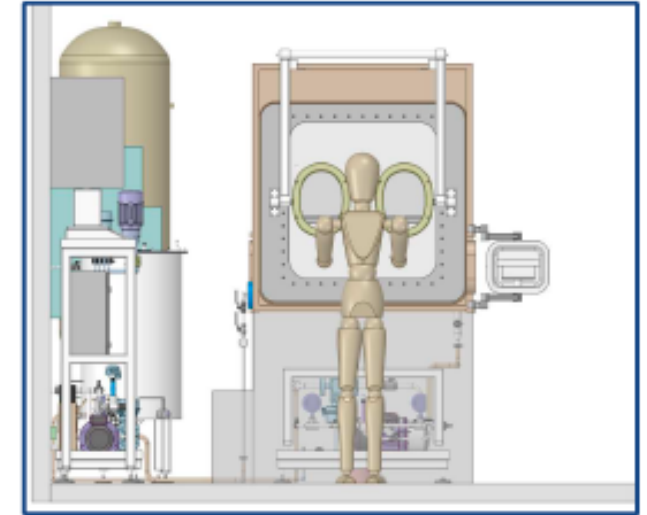
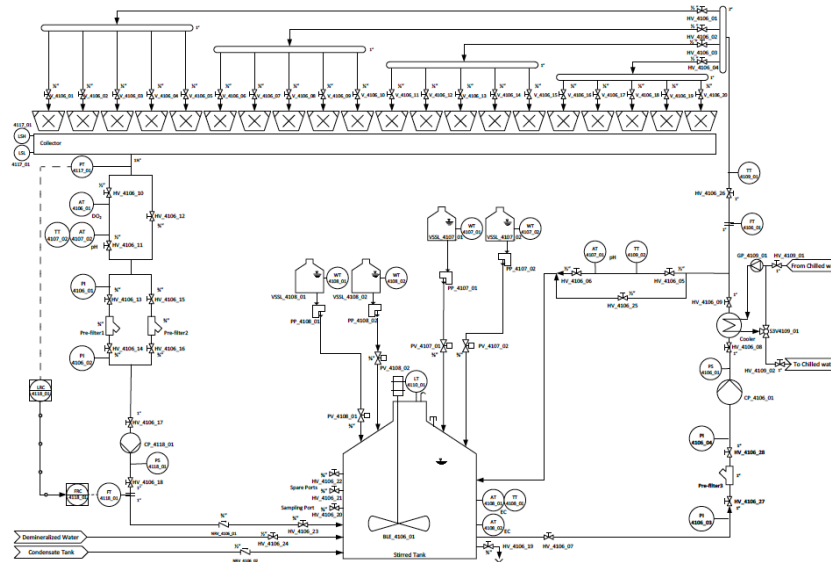
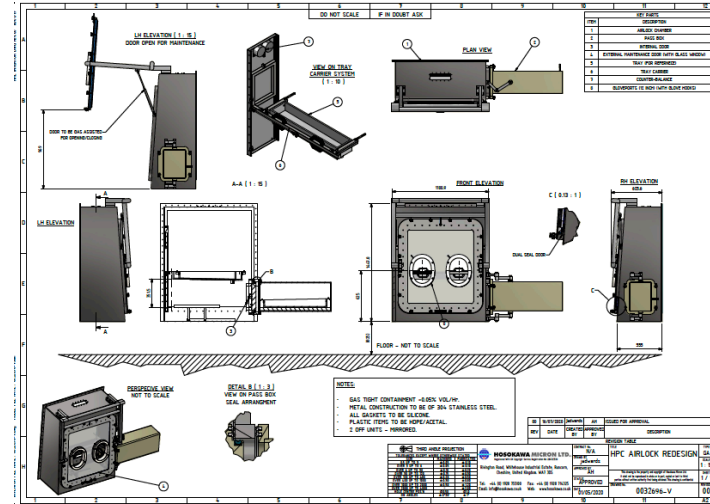
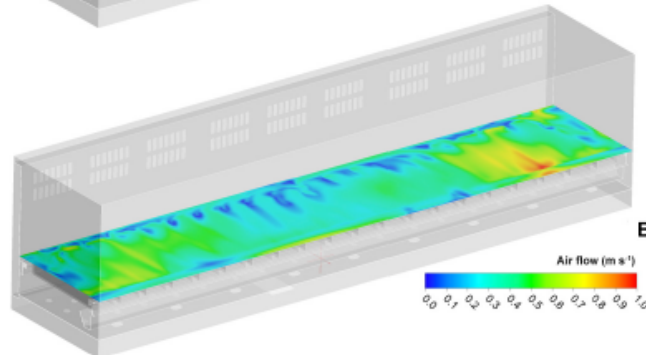
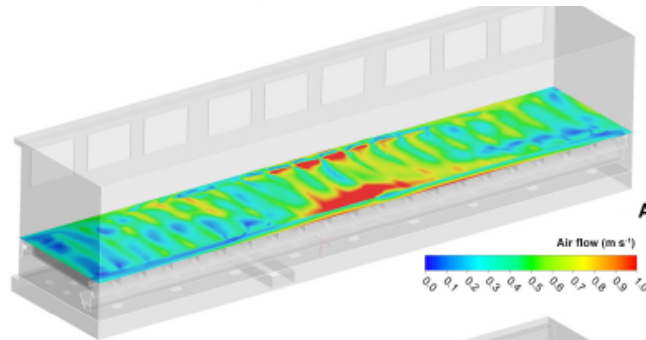
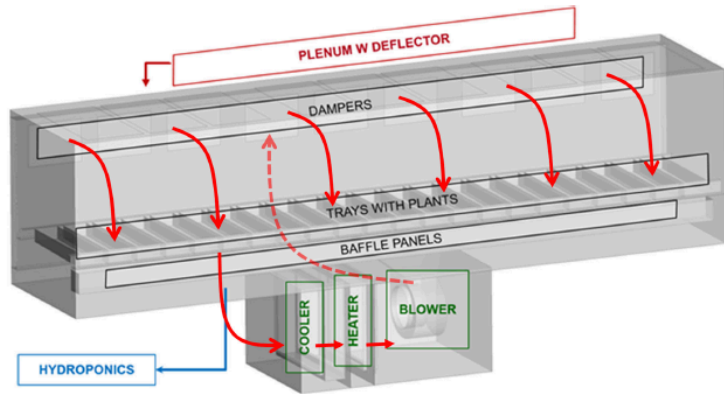
## Higher plants: lettuce, beet, wheat



## Plant Chamber

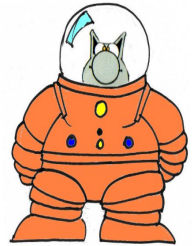


# Compartment IVb up-grade





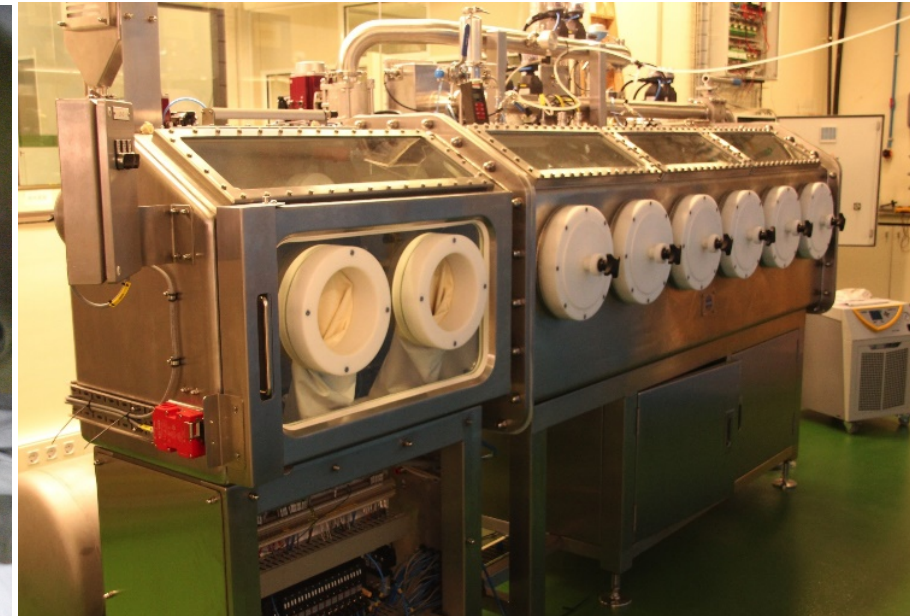
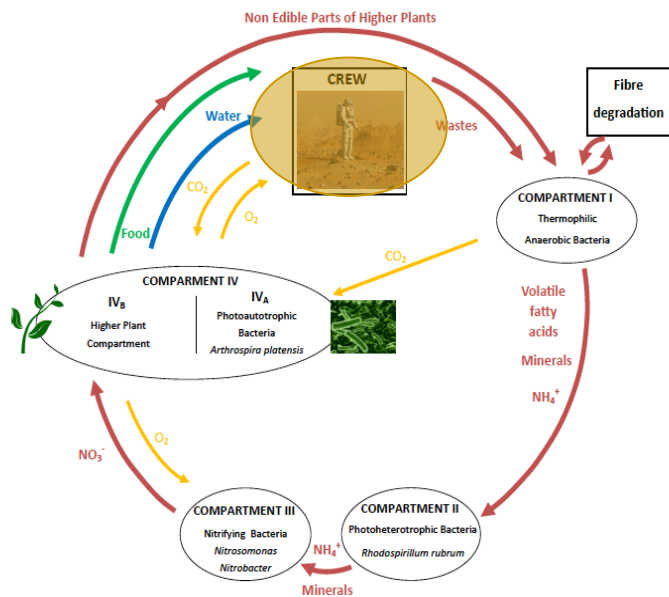
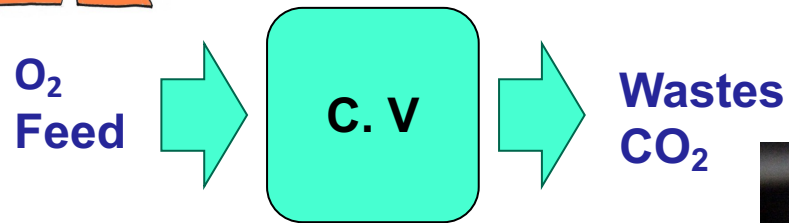
# Compartment V



Crew mock-up

Laboratory *Wistar* rats

Animal Isolator

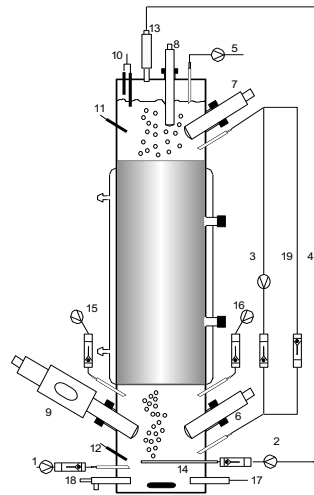


## Top requirements for the MELiSSA Pilot Plant

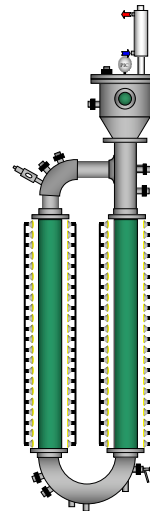
- 1/ Progressive demonstration of MELiSSA concept
- 2/ Stepwise integration
- 3/ Capitalization of knowledge



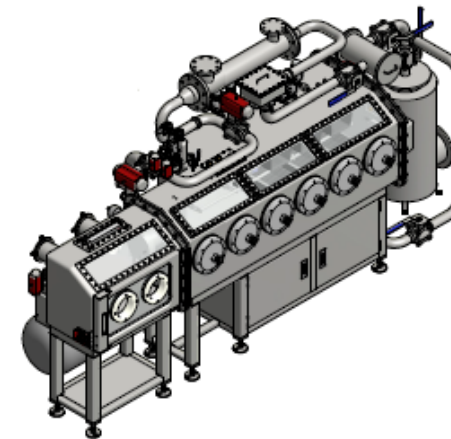
Integration logic based on the most advanced compartments in terms of knowledge, model and control



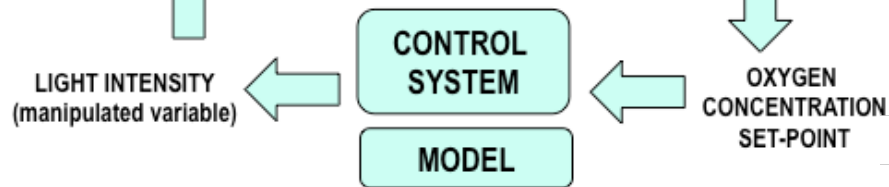
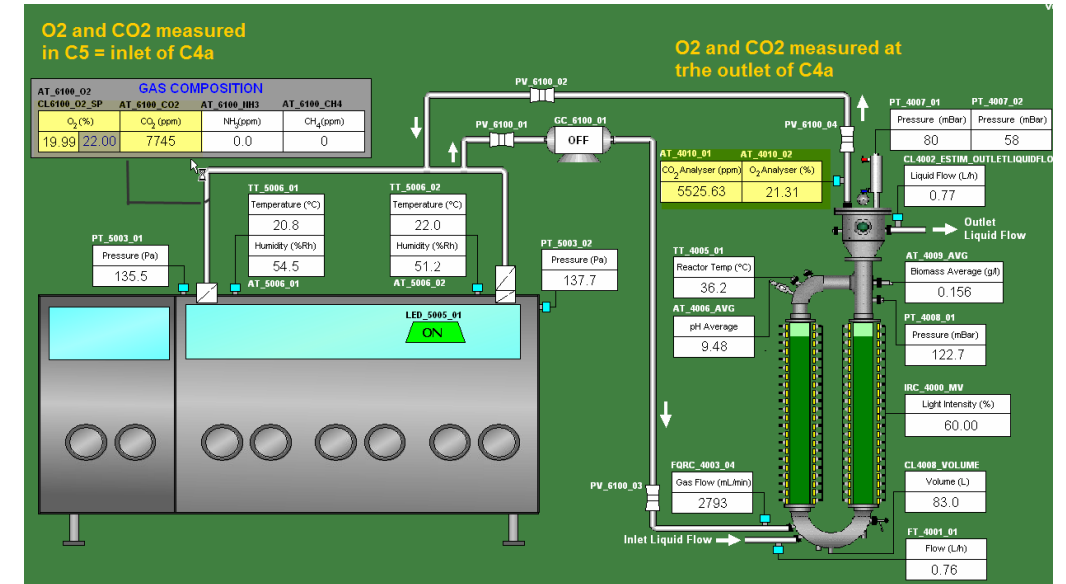
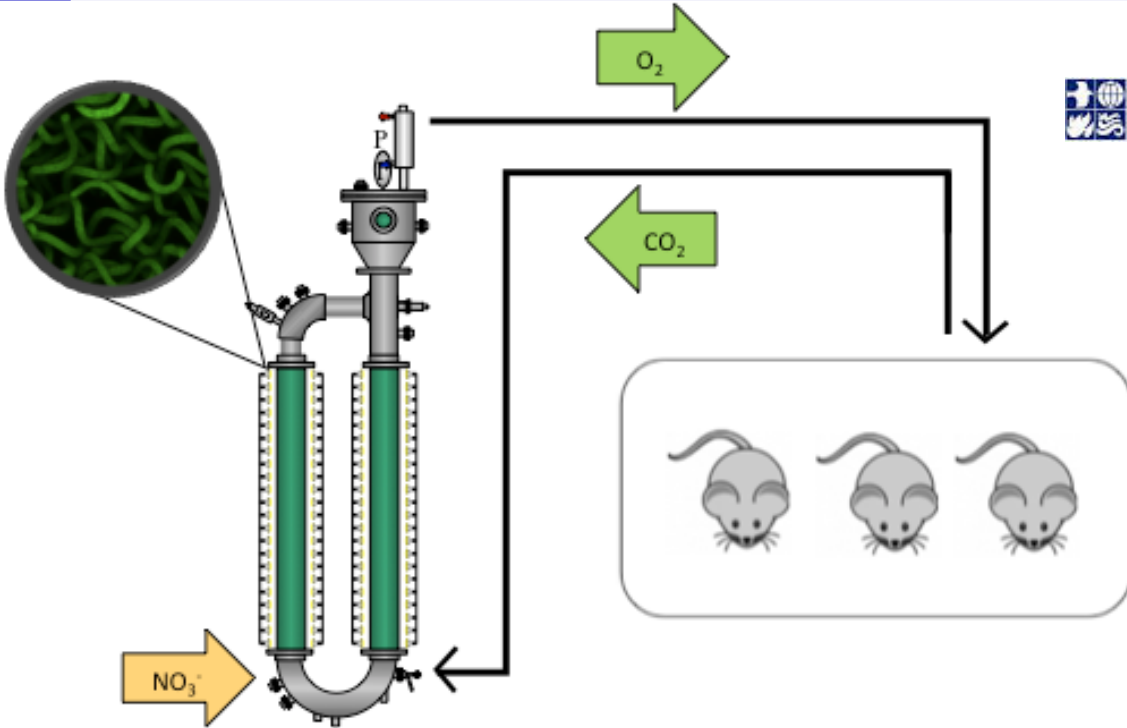
Gas  
Liquid



Gas  
Gas



# Integration of compartments: CIVa + CV connection by gas phase



**ACTIVE BIOMASS EQUATION**

$$\int_{V_i} \frac{\partial X}{\partial t} dV + v \cdot \int_{V_i} \frac{\partial X}{\partial z} dV - \int_{V_i} (\mu_{max} \cdot (X - X_{eps}) \cdot \frac{CO_2}{CO_2 + k_s} \cdot \frac{J}{p_i \cdot r^2} + \mu_{max} X_{eps} \cdot X_{eps} \cdot \frac{CO_2}{CO_2 + k_s} \cdot \frac{J}{p_i \cdot r^2}) \cdot (1 - da \cdot r_{frac}) dV = 0$$

**INACTIVE BIOMASS EQUATION**

$$\int_{V_i} \frac{\partial X_{eps}}{\partial t} dV + v \cdot \int_{V_i} \frac{\partial X_{eps}}{\partial z} dV - \int_{V_i} (\mu_{max} X_{eps} \cdot X_{eps} \cdot \frac{CO_2}{CO_2 + k_s} \cdot \frac{J}{p_i \cdot r^2}) \cdot (1 - da \cdot r_{frac}) dV = 0$$

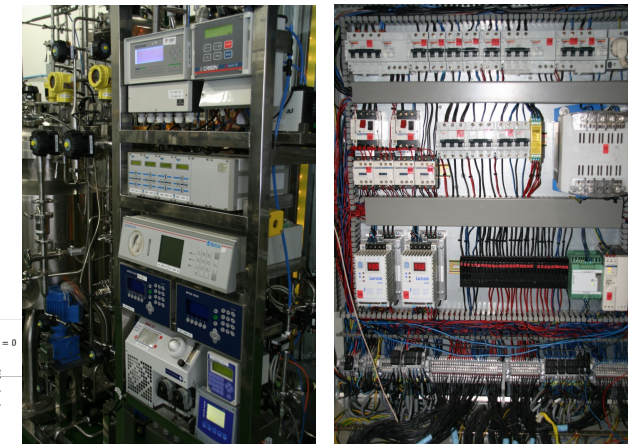
**DISSOLVED CARBON DIOXIDE EQUATION**

$$\int_{V_i} \frac{\partial C_{CO_2}}{\partial t} dV + v \cdot \int_{V_i} \frac{\partial C_{CO_2}}{\partial z} dV - \int_{V_i} (\frac{h_a}{h_g} \mu_{max} \cdot (X - X_{eps}) \cdot \frac{CO_2}{CO_2 + k_s} \cdot \frac{J}{p_i \cdot r^2} \cdot (1 - da \cdot r_{frac}) + \frac{h_a}{h_g} \mu_{max} X_{eps} \cdot X_{eps} \cdot \frac{CO_2}{CO_2 + k_s} \cdot \frac{J}{p_i \cdot r^2} \cdot (1 - da \cdot r_{frac}) + k_{1a} \cdot 0.91 \cdot (\frac{C_{O_2}}{X_1} - S_{SSSS} - \frac{C_{CO_2}}{frac}) dV = 0$$

**CARBON DIOXIDE CONSUMPTION DUE TO PHOTOSYNTHESIS**

**CARBON DIOXIDE TRANSFER TO LIQUID PHASE**

1/ Carbon dioxide  $K_{1a}$  is determined based on oxygen  $K_{1a}$ .  
 2/ Only dissolved carbon dioxide in the liquid phase is considered for the gas-liquid mass transfer.

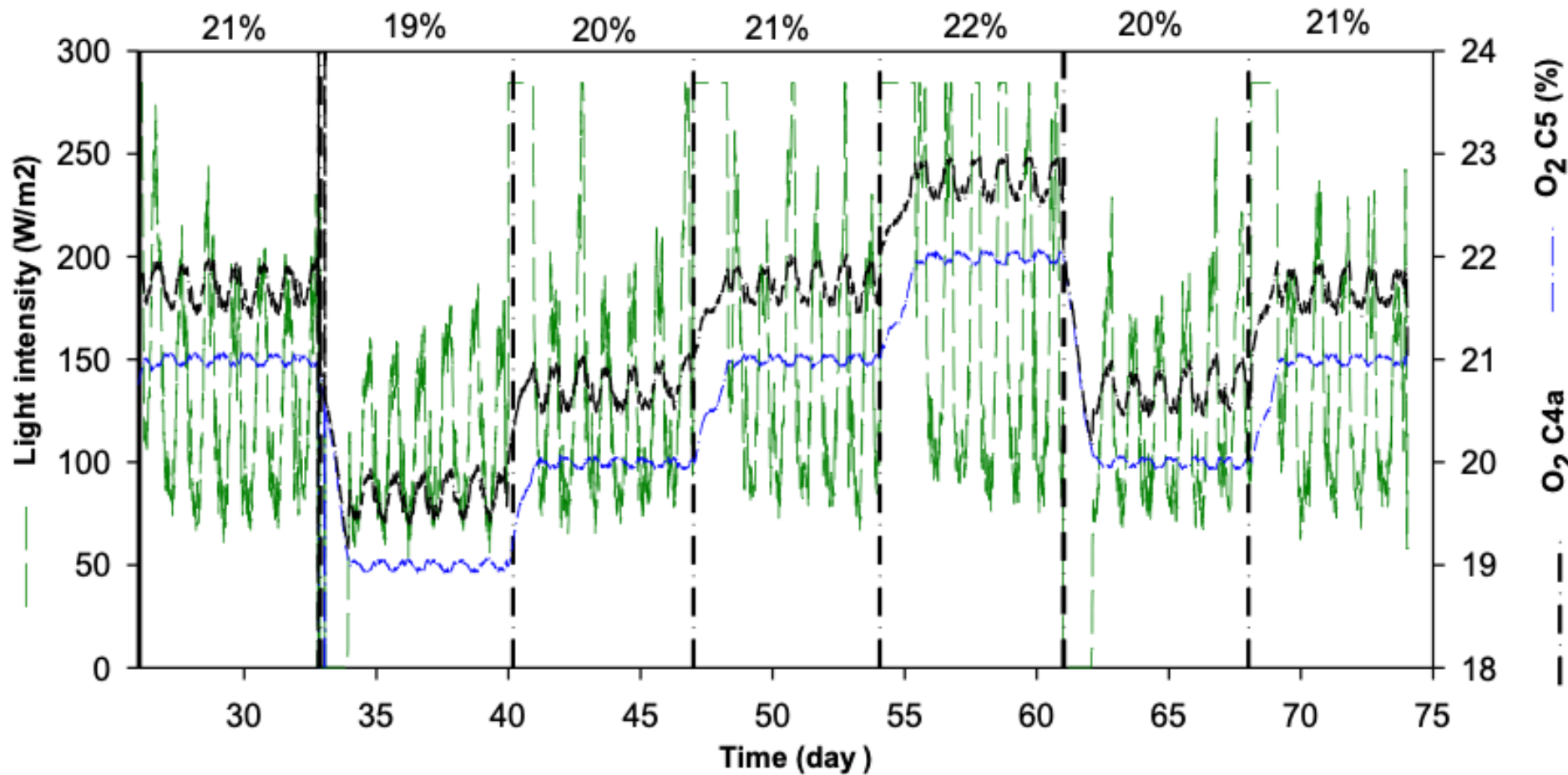




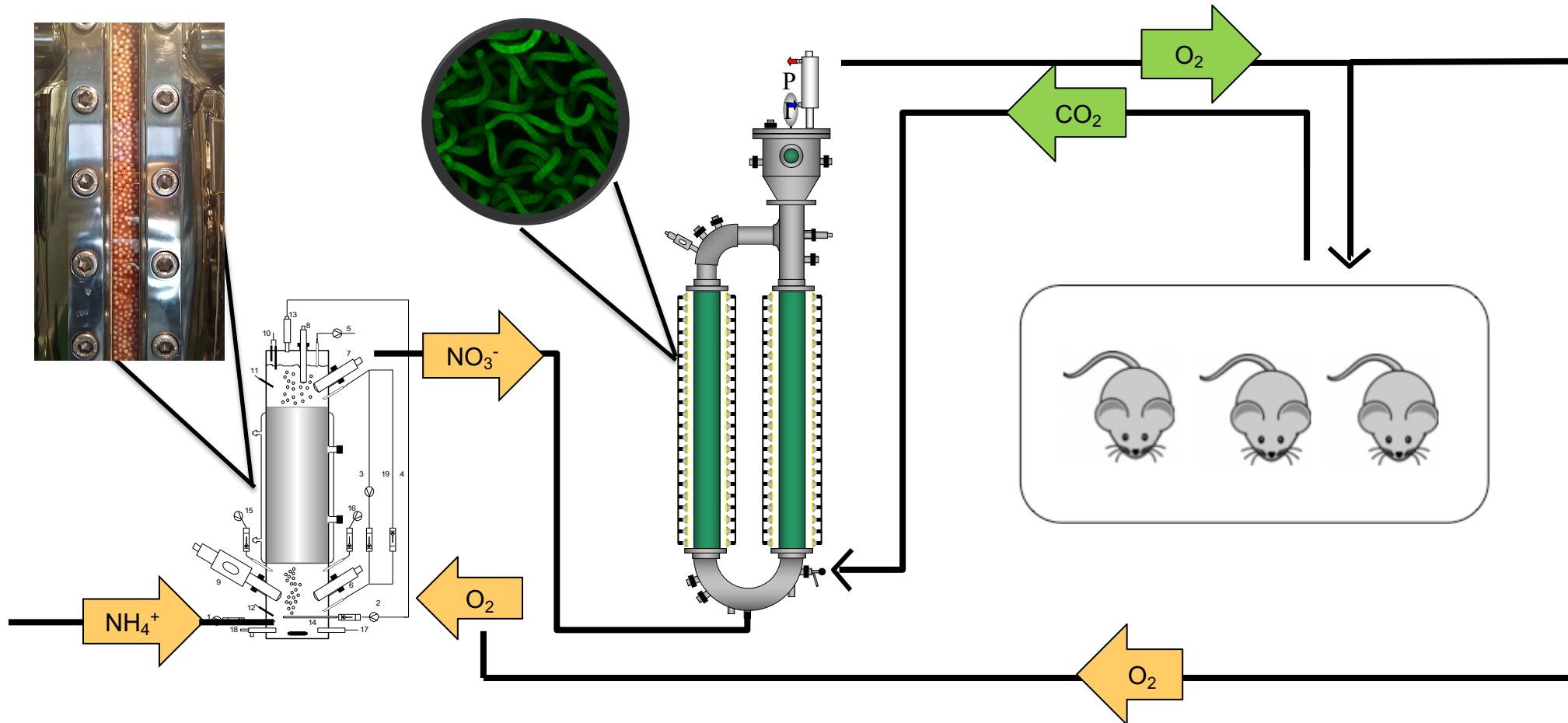
# Integration of compartments: CIVa + CV connection by gas phase



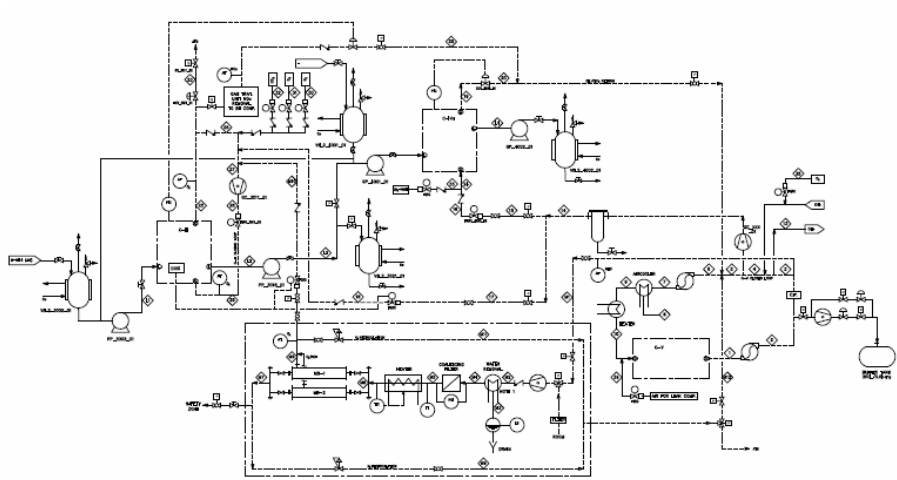
## Light and Oxygen evolution in CIVa and CV compartments



# WP6: integration of compartments: CIII + CIVa + CV, gas+liquid.



# WP6: integration of compartments: CIII + CIVa + CV, gas+liquid. (E. Peiro, Ground demonstration session)



AI	ASA	TELEIM	MAR	TELEIM	DI / AL	SPIC CREW
AI	ASA	14.12.18	MAR	14.12.18	DI/AL	SPIC CREW

**MELISSA PILOT PLANT**

Project: MELISSA PILOT PLANT

Client: ESA/UB

Contractor: HASENER

Project No: MELISSA PILOT PLANT

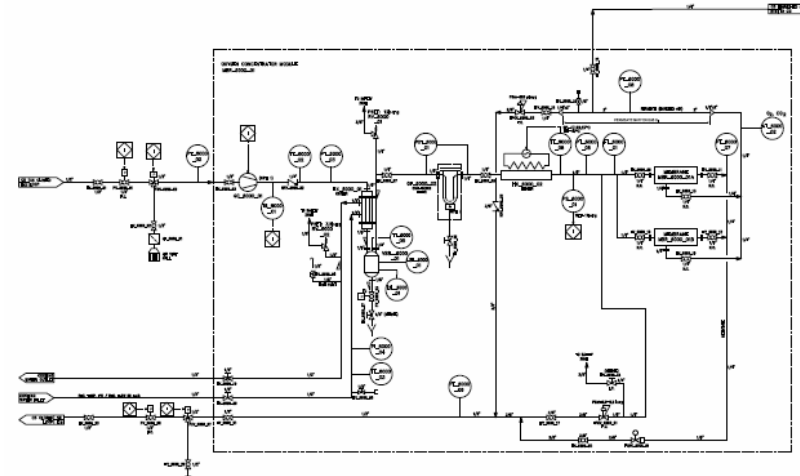
Revision: 01

Drawn By: [Name]

Checked By: [Name]

Approved By: [Name]

Issue Date: [Date]



AI	ASA	TELEIM	MAR	TELEIM	DI/AL	SPIC CREW
AI	ASA	14.12.18	MAR	14.12.18	DI/AL	SPIC CREW

**MELISSA PILOT PLANT**

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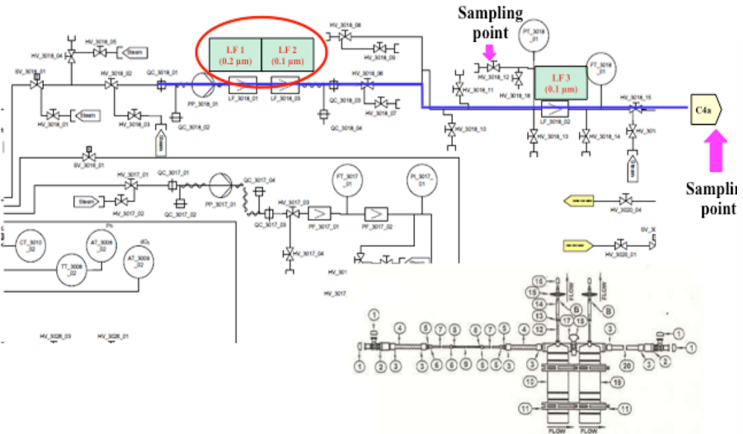
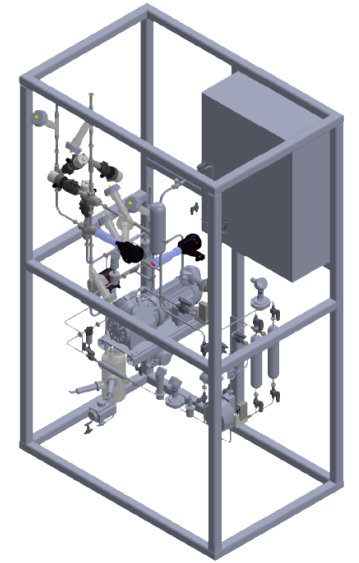
Revision: 01

Drawn By: [Name]

Checked By: [Name]

Approved By: [Name]

Issue Date: [Date]



N°	MODE *	C3 Feed Load (ppm/d)	C3 Actual Load (ppm/d)	Conv.: 93.3%	Total Air flowrate		C <sub>3</sub> Gas Phase	C <sub>3</sub> Dissolved	C <sub>3</sub> DO %	TOP SECTION		LOWER SECTION		TOTAL N <sub>2</sub>	MATERIAL BALANCE	
					(l/min)	(l/h)				R <sub>02</sub>	N <sub>02</sub>	R <sub>02</sub>	N <sub>02</sub>			
<b>NORMAL OPERATIONAL CONDITIONS</b>																
1	MODE 1	367	342	3.0	31.995	52.785	19.8	0.00800	80	0.00605	0.06245	0.37155	0.10302	0.10817	0.4797	0.4579
2	MODE 2	608	567	3.0	31.995	52.785	24.0	0.00971	80	0.00605	0.11710	0.69675	0.19319	0.20285	0.8996	0.7593
<b>MODE 1 DESIGN CASE</b>																
3	MODE 1	251	235	3.0	31.995	52.785	18.5	0.00742	80	0.00605	0.04372	0.26013	0.07213	0.07573	0.3359	0.3140
4	MODE 1	486	453	3.0	31.995	52.785	21.3	0.00855	80	0.00605	0.07992	0.47554	0.13186	0.13845	0.6140	0.6062
5	MODE 2	1286	1199	3.0	31.995	52.785	32.0	0.01288	80	0.00605	0.21847	1.29992	0.36044	0.37846	1.6784	1.6046
<b>MEMBRANE DESIGN CASE</b>																
6	MODE 2	1714	1599	3.0	31.995	52.785	38.0	0.01520	80	0.00605	0.29264	1.74119	0.48279	0.50693	2.2481	2.1380

(\*) MODE 1: LOW IN LOAD MODE ; MODE 2: OXYGEN CONCENTRATION

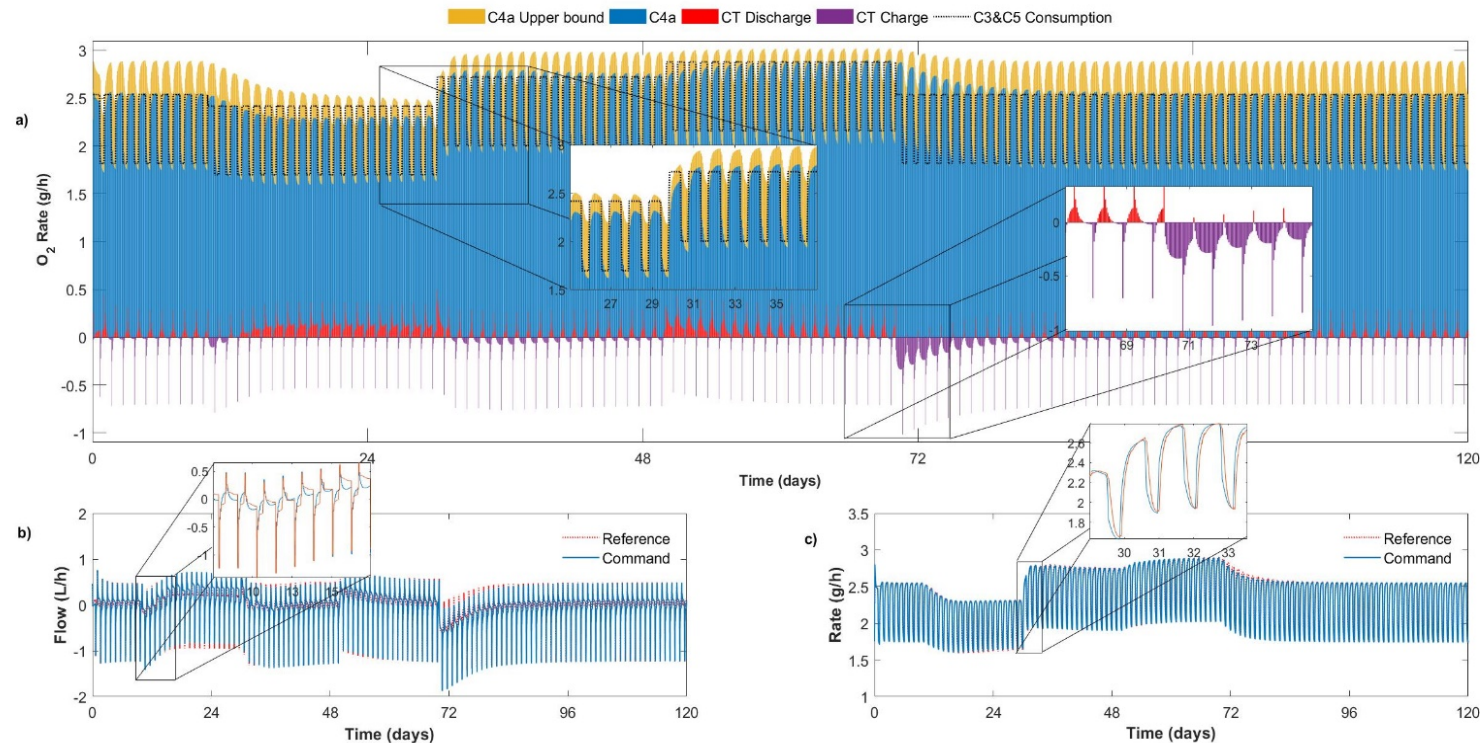
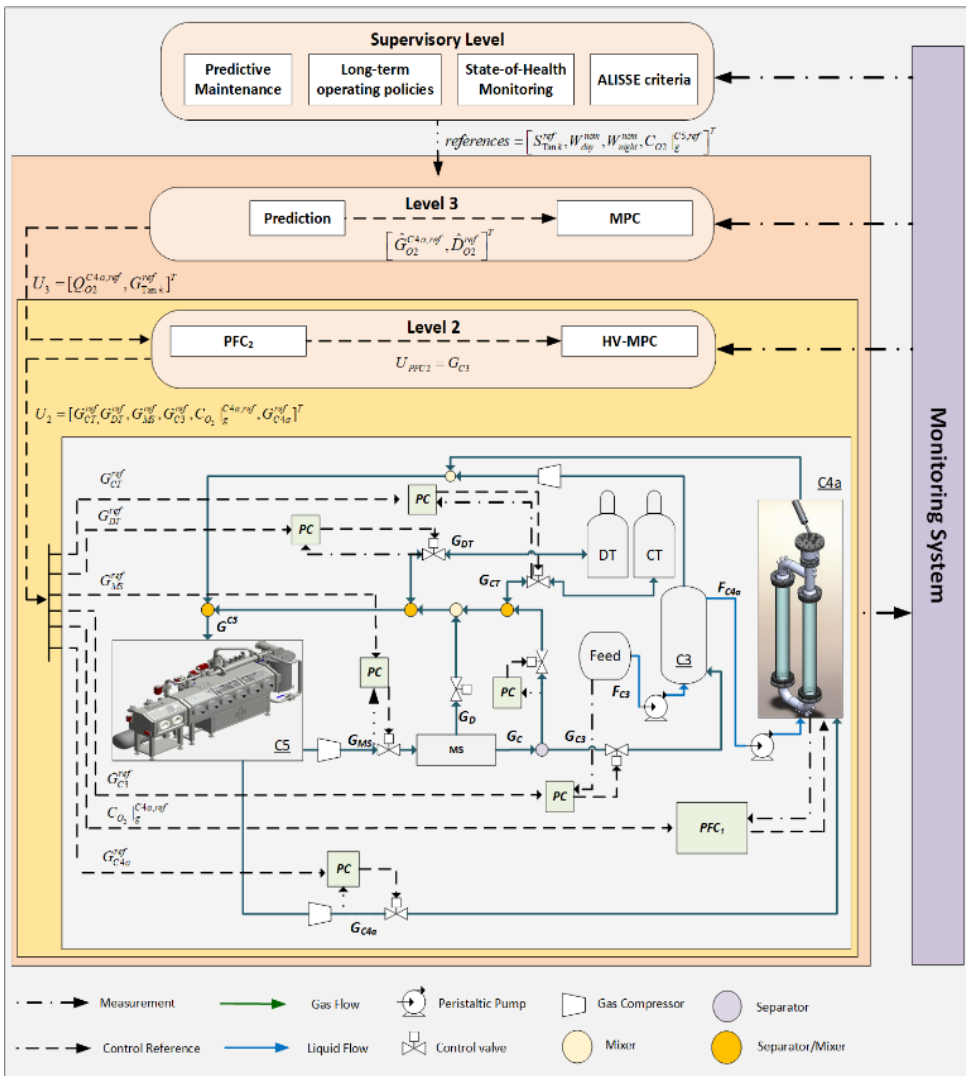




# Control architecture for the loop (C. Ciurans, poster presentation)



## Designing a hierarchical control structure for the MELiSSA Pilot Plant



# Integration of MPP: future steps



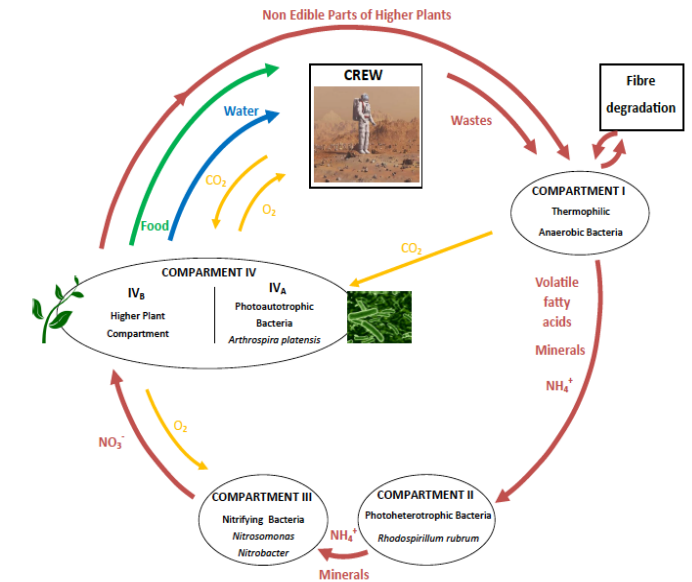
Integration of Higher Plant Chamber (gas and liquid phase)

Operation with urine

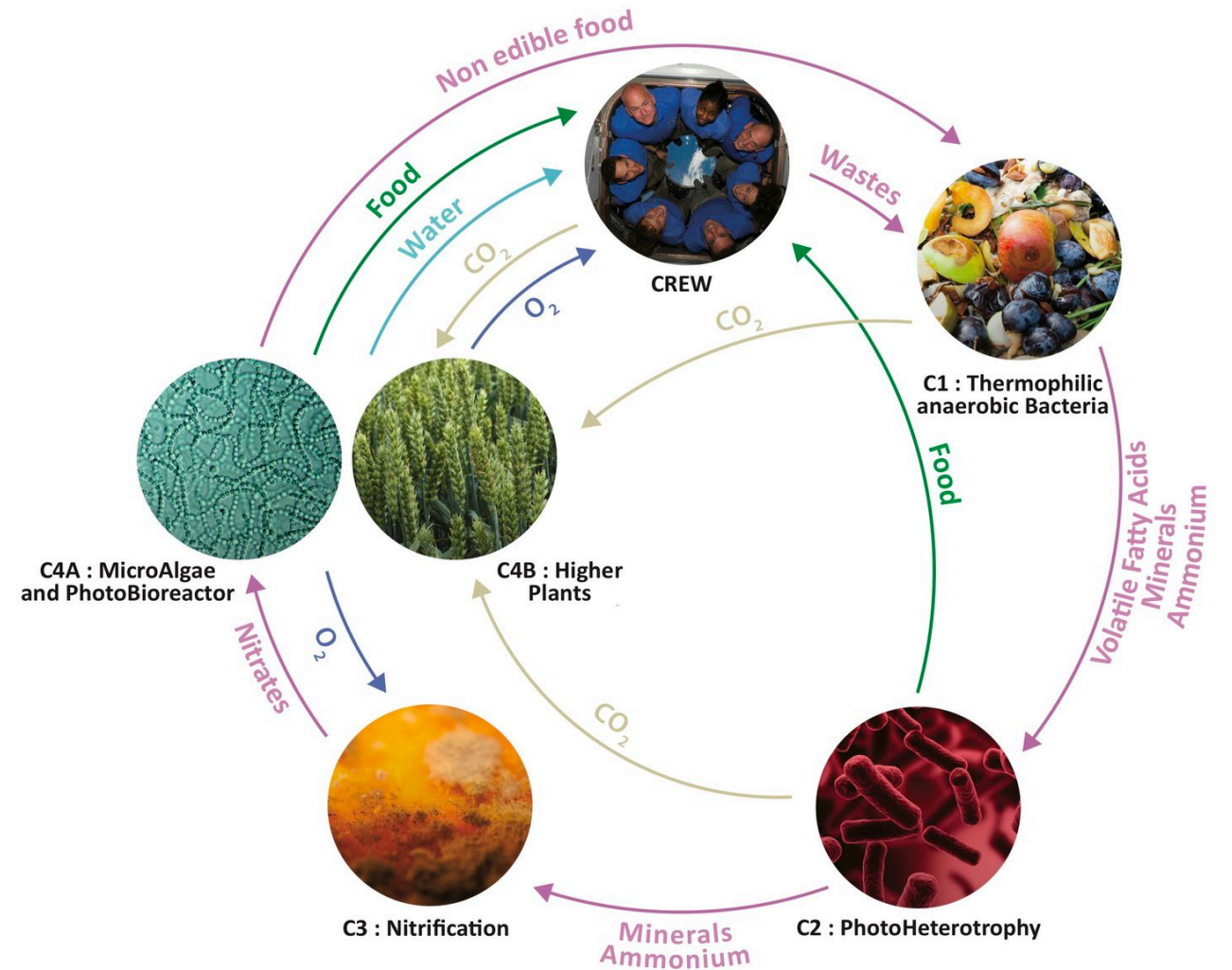
Harvest system for *Limnospira indica* (solid-liquid separation)

Integration of waste degradation technology

Final demonstration of the complete loop



# Integration of MPP: future steps





# Acknowledgements



## MELISSA Partners

ESA (EU), SCK/CEN (B),  
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SHERPA Engineering (F) ,  
University Clermont Auvergne (F)  
University of Guelph (CND),  
Université Mons Hainaut (B)  
IP Star (NL), Univ. Napoli (I)  
Univ. Lausanne (CH)



## MELISSA Pilot Plant Team

Enrique Peiro  
Beatriz Iribarren  
Carolina Arnau  
Vanessa García  
Cynthia Munganga  
Raúl Moyano  
David García  
Cristian Eslava  
Daniella Emiliani



Marcel Vilaplana  
Laura Alemany  
Jolien de Paepe  
Carles Ciurans

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## MELISSA ESA-ESTEC

Christophe Lasseur  
Brigitte Lamaze  
Christel Paillé  
Pierre Rebeyre  
Marco Volponi



# MELiSSA: from concept to a solid reality through a collaborative effort



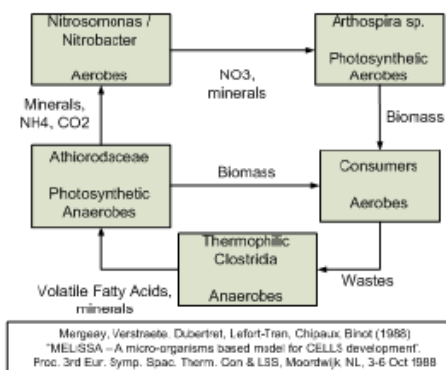
The MELiSSA Pilot Plant was dedicated on April 26th, 2011 to **Claude Chipaux (1935-2010)**, Founder of the MELiSSA Project, As a tribute to his visionary and pioneering contribution in the field of Closed Life Support Systems

*“Sur la lune, il y a des enfants Qui regardent la terre en rêvant. - Croyez-vous qu'aussi loin Il y ait des humains?”*

*“On the Moon are children Who see the Earth and wonder. - Could there be some human-kind Far away, out yonder?”*



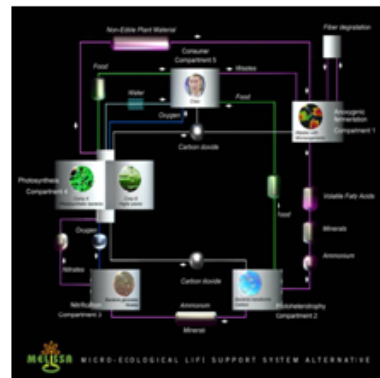
The first MELiSSA loop concept



The lake, a model ecosystem



The future MELiSSA loop...





MELISSA



MICRO-ECOLOGICAL  
LIFE SUPPORT SYSTEM  
ALTERNATIVE

**THANK YOU.**

Francesc Gòdia

*MELiSSA Pilot Plant – Claude Chipaux Laboratory*

*francesc.godia@uab.cat*

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